THE THERMAL INSULATION OF MINE AIRWAYS

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Johannesburg, 1987

**DECLARATION** 

I declare that this dissertation is my own, unaided work. It is being submitted for the Degree of Master of Science in Engineering in the University of the Witwatersrand, Johannesburg. It has not been submitted before for any degree or examination in any other University.

 $429$ (Signature of Candidate)

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#### ABSTRACT

The application of insulation material to the surfaces of airways has the potential of reducing the heat load on the ventilation air of deep mines. This study aims at assessing the viability of this technique.

Previous investigations on heat transfer from insulated airways are reviewed and are found to be flawed or out of date. A more reliable thermal analysis is presented. This shows that reductions in heat load of 50 to 70 per cent can be achieved in fully insulated tunnels, 20 to 40 per cent with partial insulation (footwall uninsulated) and less than 20 per cent with the footwall both uninsulated and Net. Nomograms are presented which predict the reduction in heat load for a wide range of conditions

An experimental study on tunnel insulation in a deep gold mine is reported. The reductions in heat load were 57 per cent with full insulation, and 30 per cent with partial insulation. These values are lower than those predicted, namely 71 and 50 per cent respectively, largely because of the uneven thickness of the insulation layer.

Guidelines are provided for the selection of insulation systems. Estimates of the financial benefits accruing from the insulation of airways are presented.

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**ONENCLATURE** 



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**MOMENCLATURE** (contd)

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L unit of length L mean beam length N interpolation matrix for finite element method Nv Nusselt number (hD/K) P barometric pressure N/mZ Pr Prandtl number (uc/k) Psat(T) saturated vapour pressure at temperature T N / m 2  $P$  'sat(T) differential of the saturated vapour pressure at temperature T  $\dot{o}$ heat flux  $W/m<sup>2</sup>$ net radiation exchange between two  $\mathbf{q}_{ij}$ nes  $W/m^2$  $\mathbf{R}$ Radius to the outer boundary whei ng to the quasi-steady method, the rock can -\*d to be at the virgin rock temperature ÷. Reynolds number (pvD/w)  $R_{\mu}$  $\overline{R}$ total thermal resistance 62.79  $\mathbf{r}$ radial dimensions  $\mathbf{T}$ absolute temperature K Ta absolute air temperature K  $\mathbf{r}$ . Tunnel heat flow function  $\mathbf{t}$ temperature  $^{\circ}$ c dry-bulb temperature \*c *t*  $\mathbf{t}_{\mathtt{ins}}$ temperature of insulated surface •c  $\mathbf{t}_e$ rock surface temperature **ec**  $t_{\rm units}$  temperature of uninsulated surface **\*c** At temperature difference **ec** U overall heat transfer coefficient W/m2K

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**NOMENCLATURE** (contd)

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#### AIMS AND CUTLINE OF STUDY

#### Introduction  $1.1<sub>1</sub>$

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Deep-level mines are characterised by high virgin rock temperatures. Traditional mining practice treats the associated high heat loads on the ventilation air as inevitable and makes use of large refrigeration plants to achieve acceptable working environments This study aims at assessing a method of reducing the heat load at source, namely by means of insulating the sain intake airways. Working depths in South African gold mines at present extend to approximately 3 600 ■ below surface, with virgin rock temperatures of up to 60 °C, and serious consideration is being given to extending operations to depths of 5 000 m, into rock temperatures of approximately 70 °C. Since 1976 the increase in heat load on mine ventilation systems has resulted in the rapid growth of installed refrigeration capacity and, as shown in Figure 1.1, is expected to continue A similar trend is evident in the cost of owning and operating refrigeration plant which at present amounts to a present value of R2 000 per kW cooling. It is therefore desirable to develop cost effective methods for combatting the underground heat load problem, and reduce the flow of heat to underground workings. Other methods of reducing the heat flow include the backfilling of worked out areas, the design of mine layouts and t.,e design of mine cooling systems

There are several sources of heat underground (for example rock, machinery, men and explosives), the most significant being that of the rock mass surrounding the workings (Bluhm et al, 1986). In particular the many kilometres of intake airway contribute a significant proportion to the overall mine heat load. This proportion grows with the life of the mine as the airways have to extend tu service the workings further from the shaft. Surface or station bulk air cooling also results in an increase of the heat load contribution by the airways, hwing to an increased temperature driving force between the air and rock One possible method of reducing the heat flow from the rock mass consists of insulating the rock surfaces

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#### 1.2 Aims of Study

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The aims of this study are to:

- (i) Conduct a theoretical analysis of the reduction in heat flow that can be achieved with both full and partial insulation of tunnel rock surfaces
- (ii) Provide for the mining industry a straightforward means of predicting the reduction in heat flow due to full and partial insulation under a wide variety of mining conditions.
- (iii) Test the theoretical predictions by experiment at an underground tunnel.
- (iv) Obtain experience in the practical problems of applying insulation to tunnel surfaces in deep level mines.

#### 1.3 Outline of Study

The metor sections of this dissertation are devoted to a theoretical study ol the heat flow reductions that can be gained by insulating rock surfaces, and to the results of actual heat flow reductions achieved at an experimental test site. However other important aspects of the analysis of the thermal insulation of mine airways have been examined.

Initially a literature search was conducted of previous work on insulating mine airways. The findings of this are presented in Chapter 2. Among the several authors who have examined the possibility of insulating mine airways as a means of reducing heat gain, most have concluded that although insulation should, theoretically, reduce the heat flow into an airway, there are no materials available which are practical for use in mines. Unfortunately the mathematical analyses were in general over-simplified, leading to errors in the estimation of the final effectiveness of the insulation. This was so mainly because neither the effect if the airway on the heat flow from the rock, nor the temperature history of the rock prior to the application of the insulation were taken into account. From this review, a more thorough analysis than any previously published appears to be warranted.

Also in Chapter 2 a review of the techniques and problems associated with evaluating heat flow into mine tunnels is presented. A knowledge of this information is essential for conducting an analysis of the heat flow reduction that can be achieved by insulating mine airways.

To mathematically assess the effect of insulation on heat flow into a tunnel, the heat diffusion equation must be solved subject to complex boundary and initial conditions.

The complex boundary and initial conditions are due to:

(i) an irregular, non-circular, tunnel cross-section;

(ii) a rock body extending to infinity;

W.

(iii) it.  $\triangle$  )<sup>\*</sup>\* boundary conditions on the rock surface, e.g. pos. partia, insulation of the perimeter; and

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(ivi the application of the insulation some time after the rock surface was exposed.

The difficulties in solving the two dimensional heat flow equation subject to these conditions were overcome by using finite element analysis or, where possible, simplified analytical approaches such as the quasi steady method (Starfield and Bleloch, 1983). The quasi-steady method was modified to allow for an insulated rock surface, and both this algorithm and the application of finite element analysis to underground heat flow problems were tested in Chapter 3. A computer program based on the modified quasi-steady method is presented in Appendix A.

Ou establishing suitable methods of predicting heat flow into insulated tunnels a theoretical study was conducted in Chapter 4. Initially each of the many parameters that effect the heat flow were examined to identify which could be assumed to be constant in the analysis. Those parameters which could nut be assumed to be constant were examined further over a range applicable to the South African mining industry.

With this information a preliminary study was conducted of the effects oi insulation on heat flow at a single tunnel cross-section. Although the results of assessing the heat flow into a single cross-section can not be applied to a mine-wide case, the mathematical procedure is simple and provides a quick and easy assessmsnt of the effects of insulation thickness, insulation thermal conductivity, the percentage covering of the rock surface and the insulation effect of the footwall ballast

This work wes then extended to allow for the effects of a finite length of tunnel The results of a large number of computer runs for varying conditions are presented in the form of nomograms

To discover the practical implications of insulating mine airways and to obtain an indication of the accuracy of the theoretical analysis a section of airway at Western Deep Level gold mine was insulated. The

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test site was divided into three 30 m sections, which were treated as  $^{\circ}$  1 lows:

- (i) Section A An uninsulated control section.
- (ii) Section  $B -$  The sidewalls, hangingwall and footwall were insulated with aouroxiaately 50 mm thick insulation foam
- $(iii)$  Section  $C -$  The sidewall and tangingwall were insulated with approximately 50 am thick insulation foam. The footwall was left untreated

Data was collected over 24 weeks and the heat flowing into the tunnel cross-sections was determined from a knowledge of the rock body temperatures and thermal properties The reductions in heat flow due to the insulation were established by comparison of the insulated section with the uninsulated control sections. These results are presented in Chapter 5

The theoretical and experimental work is compared in Chapter 6. The theoretical results were derived using finite elements which modelled the experimental test site, as closely as possible In addition a comparison was made with simple techniques of heat flow analysis and the accuracy of both methods is commented on.

Whilst the main body of work presented in this thesis is concerned with the assessment of the heat flow reduction due to the insulation, it is also appropriate to comment upon suitable materials for widescale use in underground workings. In Chapter  $7$  a breakdown of desired properties for an airway insulation is presented.

Another aspect to consider when assessing the implications of insulation is the financial savings when compared with the cost of supplying an equivalent amount of refrigeration. For this reason a financial comparison was conducted for a typical airway both with and without an insulated footwall. The resui are presented in Chapter 8. It is un fortunate that this important aspect can only be covered by a typical example, but the large number of site specific variables involved in the analysis prevent any global analysis

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In conclusion a set of recommendations have been presented as a guide to the selection and implementation of airway insulation.

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#### 1.4 Mining Terms

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In this dissertation the term 'footwall' can be considered to be the floor of a rectangular cross-sectional tunnel. Similarly the 'hangingwall' corresponds to the ceiling and the 'sidewalls' to the walls of the tunnel.

The 'ballast' is a layer of rubbie, typically 300 mm thick, placed on che footwall for laying rail tracks on.

The terms 'intake airway', 'airway', 'ventilation airway', and 'tunnel' have been used synonymously throughout this dissertation.

This dissertation reports on work carried out as part of the research programme of the Chamber of Mines of South Africa

#### *2* LITERATURE REVIEW

#### 2.1 Introduction

The aim of this chapter is to review previous theoretical and experimental studies on the effect of insulating mine airways. Since the study of heat ransfer to insulated airways has as a prerequisite the understanding of heat transfer to uninsulated airways, studies on the latter are of necessity included in the review. Chapter 3 deals in detail with the techniques of computing heat transfer to mine airways. The present chapter thus treats computational studies in outline only, with emphasis on the limitations and on the results that have been achieved, rather than on the techniques.

#### 2.2 Heat Flow into Insulated Tunnels

In simplified form the heat flow into a tunnel can be assessed by waking the following assumptions:

- $(1)$  The rock is homogeneous.
- (ii) There is negligible axial heat transfer
- $(iii)$  The initial temperature distribution is uniform throughout the rock
- (iv) The tunnel has a circular cross section.
- (v) The rock surface temperature is equal to the ambient temperature (i.e. there is no surface resistance to heat transfer).

Assumption (i), (ii), and (iii) arc not questioned in the literature, which from the experimental work of Hemp ( 1966, 1969, 1970a, 1970b) appears to be justified. In the work presented in this dissertation assumptions (i) and (ii) have been accepted, but the assumption of a uniform initial temperature distribution throughout the rock can not be made when considering events (such as the application of insulation) which occur some time after the holing through of the tunnel excavation

. is convenient to assume a circular cross-section as this facilitates an anal ;ical solution for the rate of heat transfer to be found. By

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also making assumption (v), of no surface heat transfer resistance, a solution in the form of an intractable integral is available (Nicholson, 1921). This integral was numerically tabulated by Goch and Patterson (1940), and enables a good estimate of tunnel heat flow to be simply evaluated.

An improvement on this solution was achieved when a similar integral, which made allowance for uniform surface convection, was formulated (Goldstein 1932). This integral was comprehensively tabulated (Jaeger and Chamalaun, 1966) for different Biot and Fourier numbers and similarly provides a quick and easy solution.

These two solutions are important because they have been used not only for these simple cases but as the basis of more complex problems. The solution by Goch and Patterson forms the basis of the quasi-steady method of Starfield and Bleloch (1983), which is capable of dealing with non-uniform boundary conditions, and the solution by Jaeger and Chamalaum can be used to allow for cases of uniform wetness or uniform insulation around the tunnel perimeter (Hemp, 1982).

Thus, for example the effect of a layer of insulation can be accounted for by ignoring its heat storage capacity, and calculating an effective surface heat transfer coefficient. Neglecting the very small area change due to the thickness of insulat'on x, the effective surface heat transfer coefficient  $h_{\mu}$ , is giv  $m$  by:

 $h_n = 1/(x/k + 1/h)$ 

where k is the insulation thermal conductivity and h is the surface convective heat transfer coefficient.

Most all ways in mines are approximately square or rectangular in crosssection. It is therefore desirable to derive some equivalent radius so that these simple methods may be applied. A method was devised (Wiles and Graves, 1954) from the results of an experiment making use of an electrolytic tank to study the heat flux around a square cross-section with a wet footwall. Two relationships for equivalent radii wore derived:

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 $a = b/2 \exp(-1,765+2,473F)$  (2.1)

 $a = b/2$  exp(0,795-0,940F), (2.2)

where a is the equivalent radius, b is the side of the square tunnel and F the fraction of total heat flow through the hangingwall and sidewalls. Equation 2.1 applies to the heat flux through the footwall and Fquation 2.2 to the hanging and sidewalls. It should be noted that when the footwall is totally dry (that is  $F = 0.75$ ) Equations 2.1 and 2.2 are the same, resulting in  $a = 0,547b$ .

This worx unfortunately has been misinterpreted, with most authors assuming an equal cross-sectional area relationship, resulting in  $a = 0,564$  and applying this also to situations other than totally dry. This is acceptable for the totally dry case since this relationship is close to the  $a = 0.547b$  of Wiles and Graves, but erroneous for wet or partially insulated cases.

The heat flow into a tunnel of square cross-section and partially wet surfaces has been solved numerically by Starfield and Dickson. (1967). The results of many computer runs were assembled into a data base. The wet and dry bulb t pperature increase along a length of airway is calculated by accessing the data base through an interpolation program, known as 'rapid mechod' (Starfield, 1969).

Many other simplified models have been proposed to allow for wet airways. Most of them rely on the fundamental methods previously mentioned and they have been ad-quately reviewed (Vost, 1983). Perhaps the most useful method which allows irregular boundary conditions on the tunnel circumference is the quasi-steady method of Bleloch and Starfield (1983). The basis of this method considers a thick walled, hollow cylinder with steady state heat flow conditions. The diameter of the outer wall of the cylinder varies with time so that the heat flow at the tunnel surface at any instant is equal to that of the real transient problem. In this present work much use is made of this technique in extended form so as to ac commodate partial insulation, and more detail is given in Chapter 3 and Appendix A.

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Only two authors have published heat transfer data from actual measurements taken in mine tunnels (Laabrechts, 1967 and Hemp, 1966, 1967, 1970). The work of Laabrechts was based on 305 sets of observations in mine airways, from which empirical equations for calculating wet-bulb temperature gradients as a function of air velocity and VRT were derived. His results have no direct bearing on the work in this dissertation as the equations cannot be adapted to account for the effects of insulation

Hemp (1966, 1967, 1970) produced a series of reports based on practical measurements of air and rock temperatures. The work consisted of measuring air temperatures along an airway and measuring rock temperatures to various depths at a test site. The most salient objectives of the work were to correlate observed values of heat flow with those calculated from theory, to establish values of heat transfer coefficients, and to investigate heat and mass transfer processes from a wet footwall. His results showed that it is more accurate to assess tunnel heat flow by measuring rock temperatures rather than through measuring increases in air temperature

Hemp stated

' - --:T'.

'Perhaps the most significant finding has been that the theory of heat flow into an airway surrounded by homogeneous isotropic rock provides values of the heat flow rate which agree closely with those observed by means of rock temperature measurements,'  $(Hemp, 1970)$ .

He is in fact referring to the work of Starfield (1966), with which he compared his experimental observations and obtained close agreement.

#### 2.3 Insulation of Mine Airways

The first work on the insulation of mine airways was conducted during the period 1962 to 1964 when an insulation field trial was conducted at Loraine Gold Mines Limited. This project utilized two types of insulation, namely polyurethane foam and slag wool. The heat flow was measured by drilling holes to a depth of about 3 m into the rock mass and measuring temperatures at 300 m intervals. Although a number of

measurements were made over a period of more than two years and it was found that the heat flux into the airway was reduced, the results were never published and the wide scale insulation of airways never implemented. Presumably either the results were not conclusive or the benefits not sufficiently attractive at that time.

The first documented work was concerned with the simulation of the effects of total insulation by reducing the surface heat transfer coefficient on the tunnel surface (Scott, 1959). A graph was produced showing the reduction in air temperature of an insulated tunnel when compared to that or an uninsulated tunnel

Unpublished, internal work of the Chamber of Nines of South Africa Research Organization attempted, by means of a resistance paper analogue, to quantify the \*eduction in heat flow experienced when the hanging and sidewalls are insulated Although the method was analogous to steady state heat transfer, *i\** was shown how this method could be applied to the transient problem of heat flow into a tunnel. Using the steady state analogue the radius was found at which the temperature was halfway between the virgin rock temperature and the rock surface temperature. By using the solution given by Carslaw and Jaeger (1946) for heat flow from an infinite mass to a circular tunnel it was  $possuble$  to calculate the age of the corresponding airway. The justification for this method was that the dimensionless temperature around a circular hole varies linearly for the most part with the logarithm of the radius for different values of age, and the corresponding plot for a steady state field shows the same linear relationship. This approach is the same as that applied computationally in the later quasi-steady method (Starfield and Bleloch, 1983).

Whilst the method of analysis was noteworthy, the conducting sheet pro $cedure$  was doubtful. In order to account for the layer of insulation, an equivalent thickness of rock with the same thermal resistance as the layer of insulation was evaluated. For example, a 50 mm thickness of insulation with a thermal conductivity of 0,03 W/aK is equivalent to 1,98 m of rock with a thermal conductivity of 5,6 W/aK. For a typical mine airway the effective tunnel radius was reduced to one peicent of the actual and the results are thus open to doubt.

It is possible to use the above analytical technique to calculate heat flow into a simple uninsulated tunnel without using the electrical analogue, When comparing the results of such an exercise with the results obtain... using the Goch and Patterson tables, accuracies within five per cent are obtained. It is unforturate that the results of the paper analogue were not subjected to a similar check. This would have established the validity or otherwise of the technique.

In view of this uncertainty the analogue results should be treated with some scepticism. The main conclusion was:

> 'It is considered that these benefits (reduced cooling costs) are small compared with the expense and complexity of installing and maintaining efficient insulation, and in view of this it is concluded that insulation of mines airway tunnels is not a justifiable proposition '

It is worth noting that the authors examined the decreased benefits of insulation with a finite learth of tunnel. The benefit decreases because insulation, by reducing heat pick-up, promotes a smaller air temperature gradient along the airway, thereby maintaining the temperature driving force at a higher level than in the uninsulated case. This means that estimates of heat flow reduction in an airway cannot be based on estimates referring to a single locality.

Other work conducted at the Chamber of Mines of South Africa in 1967 used an electrical analogue to study the insulation of development ends. The insulation had a conductivity of  $0.52$  W/m  $\degree$ C, which is high compared with values as low as 0,02 W/mK available for modern materials The insulation was applied six hours after exposure of the rock surface. The model assumed linear heat transfer rather than radial, and was only concerned with the heat flow during the first 20 hours from the time of exposure. The effect of cyclical wetting down of the insulation and rock surface was also incorporated While this work is not strictly relevant to long term insulation of a mine airway under dry conditions, the results show considerably lower surface temperatures as a result of inrulation.

A numerical method, based on the Goch-Patterson approach, was used to compare the temperature rise of air through  $60^{\circ}$  m of tunnel (Gould, 1968) when either completely insulated or uninsulated (with varying degrees of wetness for the uninsulated case). The results show a significant decrease in the outlet air temperature as a result of insulation, typically 1,5 °C wet-bulb The overall conclusion was that there are many practical problems which require attention before insulation becomes feasible, and that the higher the virgin rock temperatures, the more justifiable the expense of insulating. However, at the virgin rock temperatures being encountered at the time (1968) there was no merit in its application.

In more recent research some advantages of insulating airways were highlighted (Hughes, 1978). The economic benefits due to the reduction in heat flow and reduction in resistance to air flow were quantified and break-even cost figures for the insulation were evaluate . A positive case for the use of insulation was presented. Unfortunately the economic justification is erroneous due to, amongst other things, the assumption of steady state rather than transient heat flow, as we as the consideration of only one cross-section of tunnel rather than a finite length

The past work on mine insulation has generally resulted in negative conclusions with regard to its wide spread implementation. However, most of this work was either flawed or done some 20 years ago. Since then the environmental control practices in South African gold mines have changed radically. Significantly higher virgin rock temperatures are being encounteted and the widespread use of chilled service water and its natural partner - the bulk cooling of air - are well established. The available insulation materials have also changed radically over these two decades. Furthermore, the increased depths and higher rock stresses have increased the possible benefits with regard to rock support. All these factors indicate the need for a careful consideration of the insulation of mine sirways.

#### 3 COMPUTATIONAL METHODS

#### 3.1 Introduction

In this chapter the computational methods used in evaluating magnitude of heat flow from insulated airways are presented.

Initially the finite element method and the commercial computer program 'ADINA T' (Automatic Dynamic Incremental Nonlinear Analysis of Temperature), which was used extensively are introduced. The accuracy and suitability of the package were tested and the results are fully presented. The test cases described were used to derive a suitable finite element mesh configuration and time step scheme for the solution of heat flow from an infinite medium into a tunnel. A simple test of the effect of variable insulation thickness was also conducted and the results are presented.

The quasi-steady method of analysis is then described together with details of modifications which were made to accommodate the effects of partial insulation. The algorithm is then compared with the finite element method in order to assess its accuracy for a typical test case.

Finally a method for predicting heat flow into fully insulated or uninsulated tunnels is shown. The method is based on the published tables of Jaeger and Chamalaum

#### 3.2 Finite Element Method

#### 3 2 1 Introduction

The finite element method is a numerical analysis technique for obtaining approximate solutions to differential equations which occur in many engineering problems. The method was originally developed to study the stresses in airframe structures (Huebner, 1975) but has been applied to other fields such as hydraulics, dynamics and heat transfer (Desai and Abel, 1972). The attractiveness of the method lies in its ability to

handle problems having complex geometries, and boundary conditions which are seldom amenable to classical solutions (Owen and Hinton, 1990).

The basis of the finite element method is the division of the region of interest into discrete elements over which the temperatures are interpolated. The ability to specify different element sizes and shapes is one ut the most powerful features of the method. It enables the bounds'ies of the domain of interest to be modelled accurately and is capable of solving irregular meshes, which may typically have a greater density of elements at regions of greater temperature  $q<sub>i</sub>adient.$  The selection of element size, shape, and distribution is largely governed by experience. Unfortunately the accuracy of the results are often limited by the availability of computer running time or funds. A greater number of elements will tend to produce higher accuracy but will increase the use of computer resources. Typical element shapes used in commercial packages are shown in Figure 3.1. The nodal points are the positions at which temperatures are interpolated. The governing equation for transient heat conduction in two dimensions is given by

$$
k \frac{\partial^2 T}{\partial x^2} + k \frac{\partial^2 T}{\partial y^2} = \varphi c \frac{\partial T}{\partial \theta}
$$
 (3.1)

In order to solve Equation 3.1 by the finite element method, use is made of the calculus of variations (Spiegel, 1971). This variational approach leads to a functional (finotion of a function) which when minimised piovides the solution to Equation ] 1 The functional, I, for this problem is of the form (Heubner,  $1975$ ):

$$
I = \frac{1}{2} \int_{\text{Area}} \left\{ \frac{\partial T^2}{\partial x} + k \frac{\partial T^2}{\partial y} + \rho c \frac{\partial T^2}{\partial \theta} \right\} dy dx
$$
 (3.2)

The temperature distribution is then approximated by assuming:

 $T = [N]$  [T] (3.3)

 $[T]$  is a column matrix of the unknown nodal temperatures and  $[N]$  are the interpolating or shape functions which approximate the temperature behaviour throughout an element





 $\bar{\bar{\bar{\rho}}}\neq\bar{\bar{\gamma}}$ 

Substituting Equation 3.3 into Equation 3 2 and performing the relevant mathematics (Myers, 1971) to minimise Equation 3.2 produces:

$$
[C] [T] + [T] ([K] + [H]) \approx 0 \tag{3.4}
$$

where the elements of the matrices  $[C]$ ,  $[K]$  and  $[H]$  are given by:

 $R_{i,j} = k \left[ \frac{\partial N_i}{\partial x} \frac{\partial P_j}{\partial x} + \frac{\partial N_i}{\partial y} \frac{\partial N_j}{\partial y} \right] dy dx$ 

 $C_{11}$  =  $\rho C[N_1 \ N_1]$  dy dx

 $H_{i,j} = h[N_i N_j]$  dy dx

Equation 3 4 shows the relationship between the nodal temperatures and their time derivatives which must b- satisfied at each point in time to minimise I in Equation 3.2 . This system of equations is usually solved by one of the classical Crank-Micolson, or Euler (Myers, 1971) numerical difference techniques.

The computer program 'ADINA T' has been developed to solve Equation 3.4 for various boundary conditions . Comprehen ive use this program was made in assessing the heat flow from reck into a tunnel.

#### 3.2.2 The 'ADINA T' finite el ment program

The following tests were carried out in order to gain experience with the 'ADINA T' program, as well as to assess its accuracy, and to help arrive at a suitable mesh tor a partially insulated tunnel in An infinite medium.

#### TEST 1

The steady state temperature distribution in an infinitely long, thick walled pipe, subject to the following boundary conditions, as determined.

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Inside radius  $r_1 = 1,0$  m Outside radius  $r_2 = 2,0$  m Inside temperature  $T_1 = 100 °C$ Outside temperature  $T_2 = 0$  °C

The solution to this simple problem, given in many texts (Bayley et al., 1972, McAdams, 1954), serves as a useful assessment of the 'ADINA T' package.

This problem is governed by the Laplace equation, which for cylindrical co-ordinates in one dimension is given by:

 $\frac{d^2T}{dr^2} + \frac{1}{r} \frac{dT}{dr} = 0$ 

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 $\frac{d}{dr}\left(\frac{r d T}{dr}\right) = 0$ 

Successive integration leads to the general solution

\* = A In r + B

By subsitution of the boundary conditions

 $T = T_1$  at  $r = r_1$  $T = T_2$  at  $r = r_2$ 

into the general solution, constants A and B are obtained:

$$
A = \frac{T_2 - T_1}{\ln (r_2/r_1)} \qquad B = T_1 - \frac{\ln (T_2 - T_1)}{\ln (r_2/r_1)}
$$

The temperature distribution through the cylinder wall is then given b y :

$$
T = T_1 + \ln (r/r_1) [(T_2 - T_1)/\ln (r_2/r_1)]
$$
 (3.5)

IB



Inside radius  $r_1 = 1.0$  m Outside radius  $r_2 = 2,0$  m Inside temperature  $T_1 = 100 °C$ Outside temperature  $T_2 = 0$  °C

The solution to this simple problem, given in many texts (Bayley et , 1972, McAdams, 1954), serves as a useful assessment of the ADINA T' package.

This problem is governed by the Laplace equation, which for cylindrical co-ordinates in  $\rightarrow$  dimension is given by:

 $\frac{d^2T}{dr^2} + \frac{1}{r} \frac{dT}{dr} = 0$ 

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 $\frac{\mathrm{d}}{\mathrm{d} \tau} \left( \frac{r \, \mathrm{d} \tau}{\mathrm{d} r} \right) = \, 0$ 

Successive integration leads to the general solution

 $T = A \ln r + B$ 

My subsitution of the boundary conditions

 $T = T_1$  at  $r = r_1$  $T = T_2$  at  $r = 12$ 

into the general solution, constants A and B are obtained:

t \* . A . . **A.**

 $A = \frac{1}{\ln (r_2/r_1)}$   $B = T_1 - \frac{1}{\ln (r_2/r_1)}$ 

The temperature distribution through the cylinder wall is then given by:

$$
T = T_1 + \ln (r/r_1) [(T_2 - T_1)/\ln (r_2/r_1)]
$$
 (3.5)
Owing to the axisymmetric condition of the problem only one dimension need be considered when using the finite element method. However, to explore the evo dimensional features of the 'ADINA ?' package, a quarter of a planar section was analysed. The difference between an axisymmetric mesh and a planar mesh is shown in Figure 3.2, the finite element mesh used is shown in Figuy . 3.3.



Figure 3.3 Planar Finite element mesh layout for test 1.

The results from the finite element method were compared with the analytical solution given by Equation 3.5. As expected they were identical and axisymmetrical. They are not, therefore, reproduced here.

#### TEST *2*

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In order to test a convective boundary condition, a similar problem to Test 1 was set up, but with the following changes in conditions.

Inside fluid bulk temperature  $T_1 = 30,0$  °C Outside temperature  $T_2 = 45,0$  "c Inside surface convection

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heat transfer coefficient  $h = 10, 0$  W/m<sup>2</sup>K Thermal conductivity  $k = 1,0$  W/mK

With boundary conditions:

 $k \frac{dT}{dr} = h (T_{r_1} - T_t)$  at  $r = r_1$ 

By differentiating Equation 3.5 :

 $\frac{\partial T}{\partial r} = (T_2 - T_{r_1})/ln(r_2/r_1)$ 

and equating it to the boundary conditions at  $r_1$ , the inside wall surface temperature, Tr, can be obtained. Substituting this value into Equation 3 5 the temperature distribution throughout the cylinder is derived

for the finite element solution of the problem the same mesh as that in Test 1 was used. Although the results were axisymmetric, the temperatures were greater than those from the analytical solution by approximately 0,1 "C at each nodal point, This is somewhat surprising in view of the exact results obtained in Test 1, and indicates that the accuracy of the results depends on the boundary conditions for the same mesh configuration.

#### TEST 3

**解决的问题的问题,我们的理想是一个人的意思。** 

In order to assess the transient behaviour of the package the following problem was devised. A composite hollow cylinder, initially at steady state (figure 3.4), was subject to the following conditions:





Figure 3.4 Physical configuration for test 3



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 $\frac{\partial \Delta \theta}{\partial t}$ 

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Figure 3.5 One-dimensional finite element mesh layout for test 3 showing initial nodal point temperatures

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Outside surface heat transfer coefficient  $h_2 = 25$  W/m<sup>2</sup>K Densicy % specific heat gici 3,9x 106 *J / m ^ K* Density x specific heat  $Q_2C_2 = 772$ x10\* J/m<sup>3</sup>K Inside temperature 10 \*C  $30 °C$ Outside temperature ä,

At time zero a further layer was superimposed on the outer surface. The heat transfer through the compounded cylinder decayed to a new steady state solution, which was obtained analytically and served as an evaluation on the transient 'ADINA T' solution.

In the finite element ar ivsis, 18 equal length, one- dimensional elements were used (see Figure 3.5). The initial temperature distribution throughout the composite was derived analytically from the conditions given above. The overall heat transfer coefficient before superimposition is given by:

 $UA_1 = 2\pi/\sum R$ 

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 $\sum R = 1/h_1r_1 + \ln(r_2/r_1)/K_{12} + \ln(r_2/r_3)/K_{23} + 1/h_2r_3$ 

The heat flux per metre length is then given by:

 $Q/L = UA$   $(T_Q - T_i)$  W/m

Once Q/L is known the intermediate temperatures can be calculated.

The conditions specified for the superimposed layer were:





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The new overall heat transfer coefficient then becomes:

#### $U A_2 = 1 / (U A_1 + \ln(r_3/r_4) / (2 \pi k_3 t_4))$

Using the same process as before, the steady state heat flux can be calculated and hence the temperature distribution within the solid. These results were then used to assess the finite element solution.

Figure 3 6 shows the steady state analytical solution before and after superimposition and the finite e ement solutions for various time intervals after superimposition. The finite element solutions show how rapidly the transient behaviour is damped. After 10 minutes the finite element results modelled exactly the final steady state solution.

#### TEST 4

An infinitely long cylinder was surrounded by an infinite mass at a uniform initial temperature. The surface of the cylinder was suddenly reduced to a temperature T<sub>1</sub> and maintained at that value. Obtaining the solution to the heat flow at the cylinder surface is extremely important, as it ideelly represents the heat flow from rock into a tunnel

The fotm of the heat conduction equation expressed in cylindrical co-ordinates which is appropriate to the problem is:

 $k \frac{\partial^2 T}{\partial x^2} + \frac{k}{r} \frac{\partial T}{\partial r} = \rho c \frac{\partial T}{\partial \theta}$ 

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with initial and boundary conditions given by:



The solution to this problem is given by (Nicholson, 1921):

 $\dot{Q}/A = \frac{k}{r_1}$  (VRT - T<sub>1</sub>) T' W/m<sup>2</sup>

where  $T' = \frac{4}{\pi^2} \int \frac{e^{E_1 z^2}}{J_0^2 (z) + Y_0^2 (z)} \frac{dz}{z}$ 

The evaluation of T' presents considerable difficulties, but has been presented in the literature in the form of tables (Goch and Patterson,  $1940$ .

If it is assumed that:



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the heat flux over a two year period, calculated using the Goch and Patterson tables, is that given in Fig 3.7.





The 'ADINA T' package cannot incorporate an infinite element; thus the first step in sclvinq the problem is to decide on an outer boundary at which the temperature does not fall below VRT in the two year period. The relationship between rock temperature and radium at a specific time is given by (Carslaw and Jaeger, 1959):

$$
\frac{\text{VRT-T}}{\text{VRT-T}_1} = (r_1/r)^{0.5} x + \frac{(\alpha \theta)^{0.5} (r-r_1) i x}{4 \cdot (r^0)^{5} r^{1.5}}
$$

$$
\frac{\alpha \theta (9r_1^2 - 2r_1r - 7r^2) i^2 X}{22r_1^2 5 r^2 5} + \ldots
$$

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#### $X = \text{erfc} \left[ (x - x_1) / (2 / \alpha \theta) \right].$

From this expression and using the above conditions, it is found that the rock has been cooled below VRT, to a depth of 48 m.

Again this is an axisymmetric problem and a one-dimensional, 19 element, finite element mesh was used as input in the 'ADINA T' pro $q$ ram. The first element was  $0.1$  m long and subsequent elements progressed geometrically by 30 per cent, the nineteenth element being 11,25 m long. This arrangement was arrived at by trial and error, and represents a compromise between the use of computer resources and desired accuracy. The total time was split into nine intervals, each interval being progressively greater than the previous. Each interval was further split into an even number of time integration steps. The computer run was repeated for an increasing number of time integration steps

The results from the finite element solution are compared with those of Goch and Patterson in Figure 3.7. The 90-time-step solution was accurate to within 1,5 percent over the two year period and the 45-timestep solution was accurate to within 2,5 percent. The 9 time-step solution was unacceptable, differing by 7,5 percent from the Goch and Patterson solution

As a further test, the number of elements were varied for the 45-timestep solution. The results for 19,9 and 5 elements are shown in Figure 3.8, It can be seen that while 5 elements gave a very inaccurate result, 9 elements provided a quite acceptable solution. The latter was accurate to approximately 4 per cent over the two year time period.



Figure 3 3 Heat flow into a circulai tunne! from the Goch Patterson solution and from finita element analysis, using diffetent numbers of elements.

#### TEST 5

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The final test was to investigate the effect of linearly varying the thickness of a layer of insulation on a rock slab. Although this example is not a test of the features of the 'Adina T' program, the results are particularly important and are used in Chapter 6.

The assumed properties of the rock and insulation were as follows:



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Figure 3.9 Physical layout for test 5 showing the varying insulation thickness on a rock surface.

One side of the rock slab was maintained at 36 \*C and the ambient temperature on the side of the insulation was 31 "C The surface of the insulation was assumed to be subject to a convective heat transfer coefficient of  $3,2$  W/m<sup>2</sup>k. A diagram depicting the test case is shown in Figure 3 9

Using steady state analysis and a 200 element mesh it was found that there was an average heat flux of  $3.8$  W/m<sup>2</sup> from the insulated surface.

This is 20 per cent higher than if the same quantity of insulation was distributed evenly over the rock surface with a thickness of  $45$  mm.

#### 3.3 Ouasi-steady method

#### 3.3.1 Introduction

In order to solve the problem of heat flow from rock into a partially wet airway a quasi-steady method was formulated (Starfield and Bleloch, 1983). The basis of the method is that instead of attempting to soive the transient heat diffusion equation, the variation of temperature with time is neglected and the much simpler Laplace equation is solved. A hollow cylinder is assumed, with the internal radius being that of the tunnel, and the external radius receding with time. The selection of the outer radius *is such* that the thermal gradient at the internal surface matches that given by the Goch and Patterson tables. fhe mathematical formulation of the method is as follows

The solution tabulated by Goch and Patterson was for an infinitely long cylinder, surrounded by an infinite mass at a uniform initial temperature. The surface of the cylinder was suddenly reduced to a temperature  $T_1$  and maintained at this value. The form of the heat conduction equation expressed in cylindrical co-ordinates, which is appropriate to the problem, is:

# $\frac{\lambda}{\lambda r^2}$  +  $\frac{\lambda}{r}$   $\frac{\partial T}{\partial r}$  =  $\frac{\partial C}{\partial \theta}$

with initial and boundary conditions given by:

 $\theta = 0$  T = VRT or r)r  $r = r_1$   $T = T_1$  for  $\theta > 0$ 

and

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 $T \cdot VRT$  as  $r \cdot \infty$ .

The thermal gradient at the surface,  $G(t)$ , for this problem has been tabulated by Goch and Patterson. If we further assume unit thermal conductivity, unit diffusivity, initially zero temperature throughout,

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and ignore the temperate  $\cdots$  time dependence, the problem can be expressed in dimensionless form as:

 $\frac{\mathrm{d}^2\mathbf{T}}{\mathrm{d}r^2} + \frac{1}{r}\frac{\mathrm{d}\mathbf{T}}{\mathrm{d}r} = 0$ 

with  $b'$   $r$   $y$  conditions

 $T \approx$ 

and

 $T=0$  at r=R (some far boundary).

The solution is given by:

 $T(r) = [1n(R) - 1n(r)]/1n(R)$ 

for which the therma' gradient at  $r = 1$  is:

 $\frac{dT}{dr} = -1/\ln(R)$ 

If we now choose R  $\epsilon$ ; that the thermal gradient matches the true thermal gradient, G(t), we obtain

 $R = exp [1/G(t)]$ 

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The authors then assumed that, foll typical mining conditions, the position of the far boundary is insensitive to the precise form of the boundary conditions at the tunnel surface. By using finite difference methods as a comparison this was shown to be the case, except for sma.l time periods where the errors became excessive. It is therefore possible to use he quasi-steady approach to solve more complex problems by choosing an outer radius using the expression above, and solving Laplace's equation with the appropriate surface boundary conditions.

#### 3.3.2 Quasi-steady algorithm ior a partially insulated airway

The quasi-steady algorithm presented by starfield and Bleloch was for a partly wet airway and needs some modification to accommodate partial insulation. The mathematical details are given in Appendix A, with the method close:.y following that given by Starfield and Bleloch. Details oi computer program which calculates heat flux along a lengtl of airway with a partially insulated surface are given in Appendix B.

#### 3.3.3 Accuracy of quasi-steady algorithm

A test case was solved and compared With the results from a finite element analysis in order to assess the accuracy of the quasi-steady algorithm

The heat flow in a circular tunnel was evaluated as the tunnel aged from 0 to 2 years. The following conditions were assumed:



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The results of heat flow (watts per metie of tunnel length) are plotted against time for both the quasi-steady method and the finite element analysis in Figure 3.10. The results from the quasi-steady method compare favourably with those produced using finite elements, the difference being approximately 4 per cent





#### $3.4$ Simple method

The tables presented by Jaeger and Chamalaum are sufficient for analysing many of the problems of heat flow into circular mine tunnels without insulation, or with full insulation applied immediately after excavation. A computer program is listed in Appendix B which makes use of an approximation to the published tables (Gibson, 1972).

#### $3.5$ Conclusion

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 $\frac{d}{d\beta}$ 

A commercial finite element program was tested with a number of heat conduction problems which are pertinent to heat flow in tunnels. The program was shown to perform well and is used in Chapter 6 to predict the heat flow at the experimental test site.

The quasi-steady algorithm was described and mudified to accommodate partial insulation. A computer program which incorporates the algorithm is presented in Appendix 9. The results of using the algorithm compare (ivourably with the results obtained using the finite element method. The modified quasi-steady algorithm is used comprehensively in this work to assess the heat flow into partially insulated tunnels.

A computer program incorporating an approximation of the Jaeger and Chamalaum tables was  $\varphi$  esented for calculating heat flow into uninsulated and fully insulated funnels. The program is used extensively in this dissertation.

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#### 4.t Introduction

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In this chapter a theoretical analysis of the effects of insulation on tunnel heat flow is presented. The various parameters which influence heat flow are listed below and each of these was considered.

Condition of ventilation air Virgin rock temperature Tunnel age Rock specific heat Rock density Rock conductivity Tunnel radius Tunnel length Surface heat transfer coefficient Ventilation air flow rate Heat transfer due to radiation Dampness of the rock surface Insulation thickness Insulation conductivity Equivalent conductivity of footwal1 uallast Percentage covering of insulation Time of surface exposure of rock prior to application of insulation.

Each of the above parameters was examined to assess its importance on heat flow.

The presentation comprises three major parts. Initially the heat flow parameters were examined to identify those which varied but had little influence upon the heat flow into the tunnel. These patameters were then assumed to be constants. Parameters which could not be treated as constants were alro identified and methods of analysis were formulated.

The effects of insulation on heat flow at a single cross-section were then examined. The results of varying the insulation thickness, thermal conductivity and the percentage covering of the rock surface

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are described. In addition the thermal resistance of the footwall ballast was analysed.

Finally the effects of a finite tunnel length are presented. The effect of insulation is to reduce the heat flow and therefore maintain a higher temperature driving force than would be experienced in an uninsulated tunnel. The results from a single cross-section of a tunnel therefore overestimate the heat flow reduction which would be achieved in practice. Results in the form of nomograms are presented for various conditions and tunnel lengths

#### 4 2 Analysis of heat flow variables

#### 4.2,1 Tunnel age

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The importance of tunnel age on heat flow can be seen by examining the tabulated values of Goch and Patterson (See Section 2.2). The tabulated values, T', are directly proportional to heat flow, and T' is dependent upon the Fourier number, (figure 4.1) It is clear that heat flow into a tunnel varies markedly with Fourier number (and hence 'ime) for the normal lifespan of a mine tunnel. Therefore, in further analysis the effect of tunnel age was considered but limited to period of up to 10 years

When considering a long length of tunnel the age may vary considerably from the inlet to the outlet due to the time taken for excavations. It is necessary when calculating the heat flow from a length of tunnel to discretioe 'he total length into short segments, as described in Section  $4, 2, 9$ . Therefore, for the most accurate results the age of the tunnel should be replaced by the age at each segment

Two further possibilities are to assume the average age, or to make use of the logarithmic means of the ages at the start and end of the tunnel. In Table 4.1 the heat pickup from different lengths of tunnel with different development face advances is shown. It is assumed that the tunnel excavation is just complete, and that the time span between tne start and finish of the tunnel can be found from the development

face advance. The three proposed methods of calculating the age were used, namely an arithmetic mean, a logarithmic mean and an incremental increase stepwise along the tunnel It can be seen that the variation in results is insignificant and the simple option of an arithmetic mean is used throughout the dissertation

#### 4,2.2 Rock Properties

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The average values and ranges of specific heat, density, thermal conductivity and diffusivity found for quartzite in South African gold mines are shown in Table 4.2 (Jones and Bottomley, 1986).

The variation in ruck diffusivity found in South African gold mines results in a significant variation in heat flow (Figure  $4.\overline{2}$ ). Shown in figures 4 3 and 4 4 are the variations in heat flow with changes in rock density and rock specific heat respectively. It is clear that for the range of rock densities and specific heats found in South African gold mines the effect on the heat flow is negligible, and the effect of changes in diffusivity are governed by changes in rock thermal conductivity only (Figure 4.5). Further analysis assumed constant rock specific heat and density, at their average values of 777 J/kgK and  $2694$  kg/m<sup>3</sup> respectively. The effect of variation in rock thermal conductivity was examined further, with the average of 3,14 W/mK used as a standard (see Chapter 5).



#### Table 4.1 Variation is calculated heat pickup from tunnels using different *"ssumptions* to calculate age



Figure 4.1 Decay with age of heat flow into a circular tunnel

 $\frac{1}{\log n} \hat{\beta}$ 

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 $\tilde{\mathbf{z}}^{(i)}$  $\frac{\partial \mathbf{y}}{\partial \mathbf{x}}$ 

> $\hat{y}^{-1}$  $\sim$

 $\omega \neq 0$ 



**Figure 4.2** Variation of T' with time for different rock  $diffusivities$ 

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Figure 4.3 Variation of T' with time for different rock densities



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 $\hat{\mathbf{g}}^{(i)}$ 

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Figure 4 4 Variation of T' with time for different rock specific heats

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Figure 4.6 Variation of  $TT'/D<sup>0</sup>,$  2 with time for different tunnel dimensions

(4) (6) (6) 

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Table 4.2 Typical values of quar\*site properties found in South African gold mines

#### 4.2.3 Tunnel size

Mine intake airways are typically rectangular or square in crosssection. An estimate for an equivalent radius needs to be made to make use of solutions, such as that by Goch and Patterson, for heat flow into a circular cylinder. From experiments conducted in an electro- $\frac{1}{2}$ tic tank two relationships were derived for equivalent radii for square cross-sections with wet footwalls (Wiles and Crave 1954). They were



where a is the equivalent radius,  $b$  is the side of the square and  $F$  the fraction of total heat flow that flows through the hanging and sidewalls Equation 4 1 applies to the heat flux through the footwall and the significantly different Equation 2 holds for the hanging and side: walls. When conditions are uniform around the perimeter, Equations 4.1 and 4.2 become identical, resulting in

 $a = 0.547 b$ 

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 $\frac{1}{2} \rho$  $\hat{\mathcal{G}}^{(1)}$ 

> Thic is very close to assuming an equal area relationship (See Section 2 2) which results in

 $a = 0.564 b$ .

When considering the effects on heat flow due to a change in radius, it is important also to consider the change in the surface heat transfer coefficient.

The following relationship has been derived for airflow inside pipes (Dittus and Boelter, 1947):

$$
hD/k = 0.02 R_{\rm a}^{0.8}
$$
 (4.3)

or

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$$
h = 0.02 \ k(\varrho v/\mu)^{0.8}/p^{0.2}
$$

where D is the hydraulic diameter given by the ratio of the crosssectional area to the perimeter. Values of equal area radius and hydraulic diameter for varying tunnel sizes are provided in Table 4.3.

#### Table 4.3 Equivalent area radius and hydraulic diameter for different tunnel sizes



Substituting values for thermal conductivity  $k_i$ , density  $p_i$ , and viscosity w of air at 20 "C and atmospheric pressure results in

 $h = 3,63 \text{ v}^{\text{O}},8 \text{/p}^{\text{O}},2$ 

The size of intake airways are generally governed by a limiting venti lation air velocity ind it is prudent to consider that, for a change in radius, it is the air quantity that varies and not its air velocity. Considering, therefore, a typical design air velccity of 4 m/s the surface heat transfer coefficient is given by:

h =  $11,0/D^{0.2}$  (4.4)

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Introducing a surface heat transfer coefficient into the calculation of heat flux requires reference to the tables by Jaeger and Chamalaun (1966), rather than those by Goch and Patterson (1940) which assume n

infinite heat transfer coefficient. In this case the heat flow rate per unit length of tunnel is yiver by:

#### $Q/L = 2\pi\hbar r \Delta T T' W/m$  (4.5)

where  $T'$  is a function of both the Biet and Fourier numbers By substituting Equation 4.4 in Equation 4 5 it can be seen that:

 $0/L \propto rT'/D^{0.2}$ 

In Figure 4.6 the variation of  $rT'/D^{0}$ , 2 with time for different tunnel sizes is shown (the rock thermal conductivity was assumed to be 5,14 W/m"C) It is evident that tunnel site has a significant effect on heat flow and i range of sizes (Table 4.3) were examined.

#### 4.2.4 Surface heat transfer coefficient

In the previous section the expression for surface heat transfer coefficient given by Equation 4 3 was simplified to give Eruation 4.4. This was necessary fur the valuation of the effects of varying tunnel sizes. In practice the eir velocity, density and hydraulic diameter vary considerably, and it is impractical to impose limitations on the range of surface heat transfer coefficients. The surface heat transfer coefficient was evaluated for the range of conditions prevailing in practice, by means of Equation 4 3.

#### 4.2.5 Ventilation air flow rate

The design parameters for the ventilation air quantity are the tunnel size and the air velocity. A typical range of air velocities from 2 to  $6$  m/s wa. considered, 3 m/s bein; the standard value.

#### 4.2.6 Dampness of the rock surface

The only .urface considered to be damp was that of the uninsulated rock as it ia assumed that the insulation prevents moisture transfer between

the surface and the ventilation air. tness fractions' of 0,2, 0,5 and 1,0 were considered as being typic. *!* .or damp tunnels, where the wetness fraction is defined as varying from zero for a perfectly dry footwall, to unity for a totally wet footwall. A wetness fraction of  $0,2$  describes a fairly dry tunnel, whereas a wetness fraction of  $0,5$  is indicative of a damp tunnel

#### 4.2.7 Condition of ventilation air

Fur dry conditions the rate of heat flow from the rock aass to the ventil tion air is directly proportional to the difference between the virgin rock temperature and the ventilation bulk air temperature The inlet air temperature was assumed to be constant at 30 "C dry-bulb, and heat flows for other in'et temperature are easily deduced.

Heat transfer from damp surfaces was determined for relative humidities of 50 and 75 per cent at the standard dry-bulb temperature.

The influence of barometric air pressure on heat flow from the rock is negligible and a standard value of I'O kPa was assumed.

#### 4.2.8 Tunnel length

Many of the effects of insulation can be evaluated by considering a single cross-section of tunnel. In dealing with longer tunnels, lengths of up to 2 000 m were considered.

In calculating heat flow into a finite tunnel it is necessary to discretise the t \_al length into shorter segments. Heat flow into the first segment was use! to compute the air environmental conditions in the secondsegment. This process was repeated until the final segment was reached. The shorter the segment length the greater is the accuracy of the results, but with the penalty of greater computational effort. In Table 4.4 the effect of using various step lengths on calculating the heat pickup from 100 m and 2 000 m lengths of tunnel are shown. Typical mining parameters were used in the calculation, with the assumption of dry heat transfer and a tunnel age of one year.

A step length of 100 m gives adequate results, differing by less than  $2,5$  per cent from these obtained for a step length of 1  $m$ . This value was used for all further work

Table 4.4a Change in calculated heat pickup due to varying step length for a tunnel length of 100 m



#### Table 4.4b Change in calculated heat pickup due to varying step length for a tunnel length of 2 000 *m*



#### 4.2.9 Heat transfer due to radiation

In a ventilation airway hast transfer due to radiation takes place between the rock surfai , d the ventilation air, and also between the rock surfaces which are at different temperatures. The latter occurs with partial wetness or partial insulation. The overall process is shown schematically in Figure 4.7. A satisfactory analysis of the radiation heat transfer process in mine airways does not appear in the literature and is presented in detail in Appendix C. The radiation equivalent network method (Holman, 1981) was followed in the analysis.

In Appendix C it is shown that although the net heat transfer between the two surfaces in a partially insulated tunnel is relatively large, the resulting heat transfer to the ventilation air due to radiation is quite small. Nonetheless, in general the heat transfer due to radiation has been accounted for



**Surface 1**

Figure 4.7 Paths of radiation heat exhange in a ventilated tunnel.

#### 4.2.10 Virgin rock temperature

For dry conditions the rate of heat flow is directly proportional to the temperature difference between the ventilation air and the virgin rock temperature.

In Figure 4.8 the heat flow into a typical mine tunnel cross-section for varying temperature driving forces is shown. For the same set of conditions the heat flow into fully insulated and partially insulated tunnel cross-sections are provided in Figures 4.9 and 4.10. The results are expressed as percentage reductions in heat flow (Figure 4.11) and are independent of virgin rock temperature. Unless otherwise stated the virgin rock temperature was assumed to be 50  $^{\circ}$ C.

#### 4.2.11 Age of rock surface prior to application of insulation

In practice it is likely that some time will elapse from breaking new ground to the application of the insulation. It is also necessary to

Dry-bulb temperature 30°C  $10007$ Tunnel radius 1,69 m Air velocity 3 m/s 800 Heat flow (W/m) 600 **VRT 70°C** VRT 60°C 400 VRT 50°C 200  $\pmb{\mathsf{o}}$  $2,0$  $1.0$  $1,5$  $0,5$  $\circ$ Year#









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consider the importance of insulating established airways. In both these cases the rock has cooled to a certain extent prior to the insulation being applied, and the rock mass has a temperature history. This type of problem poses many difficulties and can be solved only by numerical methods. The effect will be examined closely in Chapter  $6$ for the conditions prevailing at the experimental test site.

## 4.2.12 'Standard' or average values

It may be assumed that the standards or average values have been used where all of the parameters used in an analysis have not been presented. The standard or average values are summarised in Table 4.5 along with the ranges which were examined.

PARAHETER	<b>STANDARD</b>	<b>RANGE</b>	UNITS
Age		$0 - 10$	years
Rock Density	2694		kq/n <sup>3</sup>
Rock Specific Heat	777		J/kqK
Rock Thermal Conductivity	6.14	$3,0-8,0$	W/mK
Tunnel Radius	1,69	$1, 13 - 2, 82$	霜
Air Velocity	3,0	$3,0-6,0$	m/s
Tunnel Length	1,0	$1 - 2000$	摄
Insulation Thermal Resis-			
tance	1.67	$0 - 5.0$	$m^2K/W$
Virgin Rock Temperature	50, 0		م •
Temperature Driving Force	20.0		م ہ

Table 4.5 Parameter standards or ranges for theoretical analyses

#### 4.3 Insulation at a single cross-section

### 4.3.1 Introduction

The evaluation of the heat reduction due to insulation at a single cross-section does not permit the assessment of the exact magnitude of heat flow over practical lengths of tunnel. It does, however, allow the effect of insulation thickness, insulation percentage covering and presence of the footwall ballast to be investigated.

#### 4.3.2 Insulation thickness and thermal conductivity

The most simple method of determining the effects of insulation thickness and insulation conductivity is to combine the two parameters to form the thermal resistance, given by the ratio of thickness to conductivity A good quality insulation has a thermal conductivity as low as 0,03 W/mk, and thicknesses from zero to 150 mm gives a range of thermal Assistance from zero to 5 m?K/W.

An 'equivalent' surface heat transfer coefficient  $h_{\alpha}$ , which includes the thermal resistance ' the insulation and the surface convective heat transfer coefficient  $\ldots$ , is given by:

# $h_e = 1/[\frac{$ 1nsulation thickness}{insulation conductivity} + 1/h]

The reduction in heat flow into a tunnel cross-section with varying insulation thermal resistance, compared to the uninsulated case derived from Figure 4 8, is shown in Figure 4.12. There is a clear diminishing return on increasing the thermal resistance, and obviously the optimum thickness of applied insulation is directed by financial considerations. This aspect is examined further in Chapter 8.

#### 4.3.3 Percentage covering of insulation

In practice it is difficult to insulate the footwall effectively. Although the ballast on the footwall should have some insulating effect (see Section 4.3.4), this has been ignored for the moment and the effect of partially insulating the rock surfaces has been  $\sim$  sided. The estimation c heat flow into a cylindrical tunnel wit., non-uniform boundary conditions was calculated using the quasi-steady method

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Figure 4 13 shows tie effect of varying the percentage covering of insulation. The thermal resistance of the insulation used in these calculations was  $1,67$  m<sup>2</sup> K/W. Insulating 75 per cent of the perimeter is equivalent to an uninsulated footwall. The case of 95 per cent covering may be considered as damaged insulation. It is clearly evident that it is important to have as complete a covering of insviation as possible. The effect of not insulating the footwall is

 $100 -$ 150 mm  $6,00 \, \text{m}^2 \text{K/W}$ **199 r** 3.33 m\*K/W ان، ع 50 mm **' 1.67 m \*K/W I** 60 **I** ' s **I 40-** 10 mm at 0,03 W/mK  $0.33 \text{ m}^2 \text{K/W}$ 20  $\mathbf{o}$  $\frac{1}{2,0}$ **0.5**  $1,0$  $1,5$  $\dot{\circ}$ Year:

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Figure 4.13 Reduction in heat flow for a tunnel with different insulation coverage

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severe, reducing the benefits of insulation from approximately 70 per cent to below 40 per cent. It is also important to maintain the covering of insulation, and repair wear and tear

#### 4.J.4 Thermal conductivity of footwall ballast

In Section 4.3 3 the importance of insulating the footwall was highlighted. However in practice the ballast in the footwall may provide a thermal barrier. The effective conductivity of the footwall ballast ranges from one sixth, to one half of that of the solid quartzite rock (Wiles and Maxwell, 19591

In Figures  $4.14$  and  $4.15$  the effect of the thermal sesistance of the footwall ballast on heat flow is shown. It was assumed that the ballast was 300 mm thick. It can be seen that for an uninsulated tunnel the ballast has little effect on heat flow, but when the tunnel is pacially insulated the effect becomes more significant. The reduction in heat flow for a partially insulated tunnel is approximately 35 per cent when the effect of the ballast is ignored. The reduction in heat flow rises to approximately 50 per cent if the ballast is assumed to be one sixth the thermal conductivity of the solid rock.

The effect of the footwall ballast ss exarined further at the experimental test site and the results are scribed in Chapter 5.

### 4.4 Effect of tunnel length

#### 4.4.1 Introduction

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The examination of a single cross-section of a tunnel overestimates the overall heat reduction which can be gained by insulating a finite length of tunnel. It is necessary when evaluating the heat flow over a length of tunnel to use a stepping procedure by calculating the air temperatures leaving a segment of tunnel w' ch becomes input temperatures into the next segment. This procedure is easily implemented on a micro-computer

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Figure 4.15 tunnel with different fortward ballast thermal conductivities

Results of using such a procedure for fully insulated, partially insulated, and partially insulated with a damp footwall have been presented in the form of nomograms. By adopting this method of presentation it was possible to incorporate the variation in air velocity, tunnel length and tunnel age in a single diagram. The effect of the insulation is *\** xpressed as a percentage reduction in heat flow when compared to an uninsulated tunnel.

# 4.4.2 Finite length of tunnel with the entire perimeter uniformly insulated from the time of excavation

The results of fully insulating a tunnel are shown in the nomogram in Figure 4.16. The assumed thermal resistance of the insulation is equivalent to 50 mm thick insulation with a thermal conductivity of 0,03 W/mk. The conditions described in Section 4.2.12 were assumed to apply. The nomogiam may be used to estimate the heat reductioi for varying lengths of tunnel and varying ages 45



Figure 4.16 Reduction in heat flow for tunnels with a complete covering of 50 mm thick insulation.

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As an example, consider an air velocity of  $3$  m/s for a tunnel length  $\cup$ f 2 COO m; the heat flow reduction would vary from 57 to 53 per cent as the age varies from two to ten years. Note that this heat flow reduction is not as high as indicated by investigating a single crosssection; see Figure 4.12 where the corresponding value for the age of two years is 65 per cent.

Similar nomograms are presented in Appendix D for varying insulation thermal resistance, roch conductivity and tunnel equivalent radius.

## 4.4.3 Finit length of tunnel insulated from time of exposure, with the *addwall* uninsulated

As in Section 4.4.2 the percentage reduction in heat flow for varying tunne<sup>1</sup> lengths, and differing air flows are set out as a nomogram (Figure 4 17).



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Figure 4.17 Reduction in heat flow for tunnels with a partial covering of 50 mm thick insulation.

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For the same example as before, that is an air velocity of 3 m/s and a tunnel length of *2* 000 *m,* the heat flow reduction varies from 26 to 23 per cent as the tunnel ages from two to ten years. These values are approximately half those computed for a totally insulated airway, and significantly different from those values evaluated at a single crosssection .

Further results a; presented in Appendix E for varying insulation thermal resistance, rock conductivity and tunnel equivalent radius.

# $4.4.4$  Finite length of tunnel insulated from time of exposure, with the footwall uninsulated and damp

The results for a partially insulated tunnel with a damp footwall are shown in Figure 4.18. The same procedure was followed, while addition**Welneas (actor = 0,2 Relative humidity = 50%**

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Figure 4.18 Reduction in heat flow for damp tunnels with a partial covering of 50 an thick insulation.

ally allowing for heat transfer from a wet surface. The wether factor was assumed to be  $0.2$  (equivalent to a damp footwall, that is  $24$  per cent wet) and the ventilation air at the inlet to the tunnel was assumed to have a relative humidity of 50 per cent.

Again for the same example as before, with *2* 000 m of tunnel with an air velocity at inlet of 3 m/s, the reduction in heat flow lies between 12 and 15 per cent. Further nomograms are presented in Appendix F for wetness factors of  $0,5$  and  $1,0$  and for inlet air relative humidities of 75 per cent. It is clear, however, that should the footwall be at all wet, then the application of insulation to the hanging and sidewall  $\rightarrow$ of little benefit.

#### 4.5 Summary

From an analysis of a single cross-section of tunnel it was shown that there is a clear diminishing return on increasing the thickness of applied insulation. An optimum thickness can be found from a financial analysis.

For a fully insulated finite length of tunnel it is evident that substantial savings in heat flow can be realized. A reduction in the region of 50 per cent can typically be expected.

For a partially insulated tunnel the savings are not as marked, dropping to approximately 25 per cent. This value is improved by the insulating effect of the footwall ballast

If a tunnel is only partially insulated and allowed to be damp, the benefits derived are quite small, with a reduction in heat flow of the order of 15 per cent.

The reductions in heat flow due to full and partial insulation can be estimated by reference to a set of nomograms presented in Appendix D. The nomograms cover the range of conditions found in South African gold mines and thus eliminate the need to use computer programs.

#### 5 EXPERIMENTAL INVESTIGATION

#### S .1 Introduction

Analysis of the magnitude of heat flow into insulated tunnels is extremely complex wing to the large number of variables involved. Any theoretical attempt at quantifying the flow of heat, such as that presented in Chapter 4, must incorporate many approximations. An experiment was conducted at Western Deep Levels gold mine where insulation was applied to the rock surfaces of a tunnel to check the accuracy of the theoretical results

The specific objectives of the experiment were to:

- {i ) confirm theoretical predictions of reduction in heat flow due to insulation,
- (ii) assess the effect of leaving the footwall uninsulated, and
- (iii) gain an understanding of the practicalities involved in applying insulation to mine airways

Conditions at the site were monitored for 24 weeks and the heat flow was assessed using a knowledge of the rock body temperatures and thermal properties.

#### 5 2 De scription of test

A length of airway at 9: level, 2 Shaft, Western Deep Levels Gold Mine was utilized as the experimental test site. The plan view of the test site is shown in Figure 5.1. The nominal details of the site were:



air velocity rock thermal diffuaivity rock thermal conductivity date of excavation dry rock surface no fissure water or drain water quiet site with *no* through traffic no meshing or lacing on rock walls.

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 $= 0.5$  m/s  $= 2.4 \times 10^{-6}$  m<sup>2</sup>/s  $= 5,5$  W/mK  $m$  August 1983

The total length of the tert tunnel was approximately 130 m, of which <sup>o</sup>0 **\*** were used in the experiment. The site was uated and locked at both erds to prevent interference and through traffic. The test site was divided into three 30 **a** sections, as detailed below:

Section  $A -$  uninsulated control section. Section  $B - s$  idewalls, hangingwall and footwall were insulated with approximately 50 mm thick foam. Section  $C -$  sidewalls and hangingwall were insulate  $\cdots$  roximately 50 mm thick foam. The footwall was left. , , , , ated.

This is shown schematically in Figure 5.2. Before insulating, a comprehensive set of resistance temperature measuring devices was installed in the rock mass at the centre of each section for monitoring heat flow from the rock Readings from these devices were then used to evaluate the magnitude of heat flow for each section. By comparing the results from each section the effect of insulation was assessed. Only single cross-sections of tunnel were assessed during the experiment to compute the magnitude of heat flow reduction due to insulation because

- $(i)$  the capital cost for insulation materials was kept low,
- (ii) the experiment was simple, leading to more accurate results than if a long length of tunnel was analysed,
- (iii) it was only necessary to locate a short length of underground tunnel which was suitable for the experiment.

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Figure 5.2 Schematic of insulation test site

(iv) the effect of a finite length of tunnel is easily assessed theoretically by psychrometric analysis of the changing air condition.

## 5.3 Details of Insulation

A nominal 50 mm insulation thickness was selected for the experiment. The choice was based on the theoretical analysis of the effect of varying insulation thickness (Figure 4.12). It can be seen that an insulation thickness of 50 mm results in a reduction in heat flow of the order of 70 per cent, wherees there is a diminishing return on increasing the thickness much beyond 50 mm. Blocks of 50 mm thick polystyrene foam were first bonded to the rock to serve as a guide to the required thickness of insulation foam when being applied. No other preparations were made to the rock surface (Figure 5.3). A photograph of the  $\text{dom}^+$ pleted section is shown in Figure 5.4.

Samples of the insulation were submitted to the South African Bureau of Standards for independent thermal conductivity tests. It was found that the thermal conductivity was somewhat higher than expected, namely  $0.04$ ! W/mK (density 35,7 kg/m<sup>3</sup>).

The average thickness of the insulation at the test site was computed from a total of 834 measurements. The measuremer:s for each individual section, and those for the whole site are summarised in the frequency plots (Figure 5.5). The difficulty in applying the insulation to the specified thickness is reflected both by the large scatter in the results, and in the average thickness, 76,9 *t* 31,0 mm (the standard deviation), which is much greater than the specified 50 mm. However, the average thicknesses of 74,9  $\pm$  27,1 mm and 79,6  $\pm$  35.4 mm for the Cully and partially insulated sections were similar, and permitted simple comparisons to be made.

#### 5.4 Virgin rock temperature

Knowledge of the virgin rock temperature is necessary only for purposes of comparison with the theoretical heat flow predictions. Recorded rock temperatures suffice for assessing the heat flow into the test sections.



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The test site was  $2 \times \bar{p}$  below sea level and correspondingly the virgin rock \* emperatu. . , as round in m Figure 5.6 (Jones, 1985) to be 42,7 \*C





#### 5.5 Thermal Properties of Bock from the Teat Site

The the: wal conductivity of the rock needs to be known before heat flow can be calculated. For this purpose rock samples were collected at the experimental site and analysed. A total of 35 samples from horizontal and vertical directions were taken from the airway. The values of conductivity varied from 4,56 V/mK to 6,68 V/mK with an average of  $5,48$  W/mK. The rock density varied from 2 670 kg/m<sup>3</sup> to 3 000 kg/m<sup>3</sup> with an average of 2 790 kg/m<sup>3</sup>, and the average specific heat was 912 J/kgK with maximum and minimum values of 893 J/kgK and of 765 J/kgK respectively

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SPECIFIC CONDUCTIVITY DIFFUSIVITY **SECTION** OBS DENSITY HEAT  $m^2/s$  x  $10^{-6}$  $J/kgK$  $W/mK$  $kg/m<sup>3</sup>$ 1,89  $\ddagger$ 2980 840 4,72  $1, 78$ 3000 890  $\overline{2}$  $4, 16$  $\overline{3}$ 2960 832 5.60 2,27  $2,48$  $\ddot{\phantom{1}}$ 2720 808 5,45  $\overline{\mathbf{5}}$ 2700 787  $6,06$ 2.85  $770$  $2, 19$  $\epsilon$ 797 4,75  $6,05$ 2,78 UNINSULATED  $\overline{z}$ 2700 805  $\bf 8$ 2700 806  $5.86$ 2,69  $5,95$  $2, 71$  $\ddot{ }$  $2710$ 810 10 2680 801  $5.75$  $2,68$ 2750  $807$ 2,88 11  $6,40$  $\overline{12}$ 2750 783  $2.94$  $6, 32$  $2781 + 122$  813 + 29  $5,64 \pm 0,60$  2,51 ± 0,39 MEAN  $12$ 2700 797 6,07 2,82  $\ddot{\phantom{1}}$  $\overline{2}$ 2720 807  $5.81$  $2.65$ 3000 4,55  $\overline{\mathbf{3}}$ 834 1,82  $\ddot{\textbf{4}}$ 2680 765  $5,83$ 2,84  $\overline{5}$ 2720 799 4,59  $2, 11$  $\ddot{6}$  $5,05$  $2, 29$ FULLY 2720 811 INSULATED  $\overline{7}$ 2680 786  $6,68$  $3,17$ 2670 766  $3,21$  $\bf{8}$ 6,57  $\overline{9}$ 2700 790  $6, 47$  $3,03$ 10 2720 792 4,33  $2,01$ 2,55  $11$ 2710 792 5,47  $12$ 2730  $807$ 5,59  $2,54$  $2729 \pm 87$  $796 \pm 19$  $5,58 \pm 0,81$  2,59 ± 0,46 MEAN 12  $\overline{1}$ 2920 857  $5, 63$  $2, 25$  $\mathbf 2$ 2700 802 5,92 2,73 1,78 2930 899 4,68  $\mathfrak z$  $1, 78$  $\ddot{\bullet}$ 2920 823  $4,28$  $1,93$ \$ 2910 808 4,53  $\hat{\mathbf{6}}$ 2930 863  $5,40$  $2, 14$ PARTIALLY INSULATED  $\overline{1}$ 2690 796 5,98 2.79 2,91 2740 795  $\mathbf 8$ 6,33 1,93  $\overline{9}$ 2930 808 4,56 2930 4,64 10 838 1,89  $11$ 2970 832  $4,88$  $1,97$  $5, 17 \pm 0, 71$  2, 19  $\pm$  0, 42 MEAN  $11$  $2870 \pm 104$  829 ± 33 OVERALL MEAN 35  $2791 \pm 118812 \pm 30$  5.47  $\pm$  0.722.43  $\pm$  0.45

#### Table 5.1 Rock Thermal Properties

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When calculating the heat flux from each section the average thermal properties for that section were used and not the overall average values given above. The complete set of measured values is shown in Table 5.1.

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#### 5.6 Cross-sectional Dimensions

The dimensions of the tunnel cross-sections at each of the measuring stations were measured for each of the four rock faces. The results are shown in Table 5.2. The texture of the rock faces varied from smooth to fragmented. The cross sectional shape was approximately rectangular





#### 5.7 Air temperature Measurements

The heat flow into each section was evaluated from the m. sured rock temperatures, a knowledge of the rock thermal conductivity and the mechanics of two dimensional heat flow. The change in energy content of the air passing through the section was not used to determine heat flow from the rock because air temperatures and airflow cannot be measured with sufficient accuracy.

The heat flow into a typical dry mine haulage is 150 W/m, so that over 30 m of airway the total heat flow is 4,5 kw For an air mass flow rate of 20 kg/s the temperature increase over the section would be 0,2 "C, with temperature change in the ir.ulated sections being much less. Measuring changes in temperature of this magnitude to a suitable degree of accuracy, at an underground site, is almost impossible.

However, the wet- and dry-bulb air temperatures were monitored continuously at the test section exit. A chart recorder which was calibrated weekly against an accurate thermometer members was used for this purpose. The dry-bulb temperature was found to be constant at apprcx mately 31  $^{\circ}$ C, varying by only  $t$  1  $^{\circ}$ C during the experiment. The wet-bulb temperature varied from 22 °C to 26 °C, but was not considered important as the airway was completely dry.

## 5.3 Air Velocity

The air velocity at the outlet of the test section was recorded on a weekl, basis using a hand-held anemometer. The results were computed from an average of five readings taken at different points within the duct cross-section. It was found that the air volume varied greatly over the period of the experimer... (Figure 5.7). This resulted in significant variations in the magnitude of the measured heat flow.



Figure 5.7 Variation in ventilation air flow.

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The accuracy of the air velocity measurement was not high, with an expected error of between five and ten per cent. This level of accuracy was however adequate since an energy balance technique was not used to evaluate the heat flows, and the results of air flow measurement were used only to indicate the effect on heat flow, and to evaluate a surface heat transfer coefficient for theoretical comparison purposes.



## 5.9 Rock Temperature Measurements

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The sensors used to measure rock temperature were resistance devices  $(R, T, D's)$ . Creat care was taken to protect the sensors from damage by the environment. Each device was sealed in neoprene and then, to make up a probe, inserted into a plastic tube. The probe assembly was com- pleted by positioning flexible plastic baffles at abort intervals along the length of the outer plastic sheath. The diameter of the baffles was slightly larger than the holes in the rock, the purpose being to form an interference seal and thus prevent convection currents within the hole. A schematic of the temperature probe is shown in Figure 5.8 and the electrical circuit diagram is shown in Figure 5.9. Prior to inserting the probes into the holes in the rock the holes were cleaned of all drilling water by blasting with compressed air.

Each sensor was calibrated after assembling, so that the resistances of leads and connections were included in the calibration. The expected error in temperatures recorded was less than  $\pm$  0,2 °C.



Figure 5.10 Distribution and pattern of temperature measuring points

The probes were installed at the centre of each section (A,B,C) in holes drilled to a depth of 6 m (Figure 5.10). Also shown are the positions of each sensor. If should be noted that the sensors were pla:ed closer together near the surface than deep in the rock, to enable detailed information to be gained for the localities where the temperature gradients were largest. The entrances to the holes were were tested immediately after installation, and then left for one week before regular weekly measurements commenced.

filled with putty to further prevent convection currents. The sensors<br>
were tested immediately after installation, and then left for one week<br>
before regular weekly measurements commenced.<br>
Some typical rock temperature pr Some typical rock temperature profiles recorded at the start of the ^ experiment and 24 weeks later are shown in Figures 5.11 to 5.16. Results from every second temperature probe are shown and several ^ points of importance should be noted. ^

- (a) At the uninsulated section the gradients close to the surface were steeper than for those of the insulated section; this indicates a higher heat flux at the uninsulated section than at the insulated  ${\bf s}$ ections .  $\mathbb{R}^N_{\geq 0}$
- (b) The temperature profiles for the uninsulated section changed little over the 2? week period, particularly deep in the rock where the temperature ignained essentially constant at 37  $^{\circ}$ C.

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- (c) At the insulated rock faces the temperature profiles were relatively flat with a low thermal gradient at the surface and a correspondingly low heat flux. There was a general increase in temperatures over the 24 week period due to the reduced heat flow across the rock and air interface
- (d) The temperature profile at the uninsulated rock face in the partially insulated section showed characteristics found in the uninsulated section; namely that of a high thermal gradient which is indicative of a high heat flow.

The low scatter of the data points lying on the temperature profiles suggests that random errors were low

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Figure 5..1 Rock temperatures in the uninsulated section during<br>Week 1

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Depth (m)

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Temperature (°C)  $\mathbf{30}$ 

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Figure 5.12 Rock temperatures in the uninsulated section during<br>Week 24.

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Figure 5.13 Rock temperatures in the fully insulated section during Week 1

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Figure 5.14 Rock temperatures in the fully insulated section during Week 24



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Figure 5.15 – Rock temperatures in the partially insulated section<br>during Week 1

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Rock temperatures in the partially insulated section<br>during Week 24. Figure 5.16



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Figure 5.18 Temperature contours at the fully insulated section

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Temperature contours at the partially insulated  $section$ 

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Typical temperature contours around the tunnel sections are shown in Figures  $5.17, 5.18$ , and  $5.19$ . Again several points should be noted.

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- (a) The uninsulated and fully insulated sections having uniform boundary conditions show almost symmetrical and concentrical temperature contours.
- (b) The rock temperatures around the fully insulated section are higher than those around the uninsulated and partially insulated sections.
- $(c)$  The high rate of heat transfer through the footwall of the partially insulated section is indicated by the divergence of the temperature contours away from the footwall.

5.10 Heat Flux

#### 5 10.1 Method of calculation

The heat flux was found by determining the temperature gradient at the rock surface from a curve fit (both the radial and circumferential dimensions were considered). By using this approach only the rock temperatures and thermal conductivity are necessary to obtain the surface heat flux.

It was not possible to fit one equation to all  $48$  temperature measurements taken at a section due to the discontinuity of the hole formed by the tunnel in the rock mass. The method used was to iit four curves over segments around the tunnel perimeter. Each segment included temperature recordings from three probes, giving a total of eighteen temperature measurements (Figure 5.20). For example, a cur was fitted within the buundary, outlined by segment 1, from temperature recordings from probes 1,2 and 3. The curve fit for segment 2 was from temperature recordings from probes 3,4 and 5. A quadratic of the form

#### $T = a_1 + a_2 x + a_3 x^2 + a_4 y + a_5 y^2 + a_6 x y + a_7 x^2 y + a_8 x y^2 + a_9 x^2 y^2$  (5.1)

was fitted to the temperature data in each segment using a modified least squares method (Hurlburt, 1980).



Position of four segments over which curve fitting<br>was performed Figure 5.20

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The dimensional co-ordinates  $\geq$ re given by x (parallel to the rock face) and y, (normal to the rock face) and the temperature in the rock body by T. The error at the measuring points using the quadratic fit was less than one per cent in all cases.

The heat flux normal to the surface was then obtained from

$$
\frac{k}{\partial y} \frac{\partial T}{\partial y_{y_{27}}}\approx k(a_4 + a_6 x + c_7 x^2)
$$
 (5.2)

After determining the variation in heat flux around the perimeter the total heat flow at each section was found by integrating Equation 5.2 for each section, that is

Heat flux = 
$$
\frac{k}{L} \int_{0}^{L} (a_4 + a_5 x + a_7 x^2) dx
$$
 (5.3)

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where L is the langth of the side.

## 5.10.2 Heat flow from eich section and percentage heat flow reduction

The total heat flow from the three test sections for the duration of the experiment are given in Table 5 3, and presented graphically in Figure 5.21. Also shown in Table 5.3, and plotted in Figure 5.22, are the percentage reductions in heat flow for the fully insulated and partially insulated cases. The raw data were then smoothed using a cubic spline fit and plots of the heat flow and percentage heat reduction are shown in Figures 5 23 and 5 24

The average heat flow from the uninsulated section wis  $80,6 \pm 11,1$  W/m, whereas for the partially and fully insulated sections the average results were 34,6  $t$  4,5 W/m and 56,0  $t$  6.1 W/m respectively.

The average reduction in heat flow as compared with the control section, was 56,7 per cent in the totally insulated section and 29,7 per cent in the partially insulated section.



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Figure 5.21 Variation in heat flow for insulated, partially insulated, and fully insulated sections

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Figure 5.22 Percentage reduction in heat flow due to full and partial insulation



Variation in heat flow for insulated, partially<br>insulated, and fully insulated sections (smoothed) Figure 5.23

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Figure 5.24 Percentage reduction in heat flow due to full and partial insulation (smoothed)

# 5.10.3 Heat flux variation around section perimeters and the effect of vaiiations in air flow

Typical results for the variations in heat flux around the perimeters of each section are shown in Figure 5,25. In the uninsulated section the heat flux around the rock perimeter varied from 3 to 7  $W/m^2$ . This variation was greater than that in the fully insulated section which only varied from 2 to  $3.5$  W/m<sup>2</sup>. The heat flux in the partially insulated section increased from 2,5 W/m<sup>2</sup> at the insulated hangingwall, to  $7.5$  W/m<sup>2</sup> at the centre of the uninsulated footwall. The sidewalls in the partially insulated section showed a steadily increasing heat flux from low at the corners adjacent to the insulated hangingwall, to high at the corners next to the uninsulated footwall.



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Table 5.3 Heat Flows for the Uninsulated, Fully Insulated and Partially Insulated Sections



Figure 5.25 Typical heat flux variation around the tunnel perimeters during Week 22

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Figure 5.27 Variation in heat flux for fully insulated section (smoothed)



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Figure 5.28 Variation in heat flux for partially insulated section (smoothed)

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The variations in heat flux with time for the individual sidewalls, hangingwells and footwalls are shown in Figures 5.26, 5.27 and 5.28. The data were smoothed using the cubic spline fitting technique. The highest average heat flux,  $6,2 \pm 0.5 \sqrt{m^2}$ , of all rock surfaces was recorded from the uninsulated footwall in the partially insulated section.

This was caused by heat transfer along the path of least resistance which is away from the insulated faces and through the uninsulated footwall. This high heat flow indicates the importance of using a suitable material to insulate the footwall.

The large variation in heat flux for the uninsulated section (Figures 5.21 and 5.26) can be explained by the variation in air volume flow rate (Figure 5.7). The sharp reductions in air volume, and hence air velocity, at the 5 to 7 and 15 week periods (Figure 5.7) correspond closely to the drop in heat flux at the 6 to 8 and 16 week periods (Figure 5.21). The variation in air volume resulted in a change in air velocity passing over the rock surface and consequently a variation in the convective surface heat transfer coefficient. The fluctuations in heat flow in the insulated sections were much less because the rate of heat transfer is dominated by the thermal resistance oi the insulation, and is less dependent on the surface heat transfer coefficient.

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The response in heat flow to changes in air flow was investigated by stopping the air flow completely and recording temperatures daily for



Figure 5.29 Variation in heat flow for 5 days after stopping ventilation air flow.

The variations in heat flux with time for the individual sidewalls, hangingwalls and footwalls are shown in Figures 5,26, 5.27 and 5.28. The data were smoothed using the cubic spline fitting technique. The highest average heat flux,  $6.2 \pm 0.5$  W/m<sup>2</sup>, of all rock surfaces was recorded from the uninsulated footwall in the partially insulated section.

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The response in heat flow to changes in air flow was investigated by stopping the air flow completely and recording temperatures daily for



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Figure 5.29 Variation in heat flow for 5 days after stopping ventilation air flow.

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The variations in heat flux with time for the individual sidewalls, hangingwalls and footwalls are shown in Figures 5.26, 5.27 and 5.28. The data were smoothed using the cubic spline fitting technique. The highest average heat flux,  $6.2 \pm 0.5$  W/m<sup>2</sup>, of all rock surfaces was recorded from the uninsulated footwall in the partially insulated section.

This was caused by heat transfer along the path of least resistance which is away from the insulated faces and through the uninsulated footwall. This high heat flow indicates the importance of using a suitable material to insulate the footwall.

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The response in heat flow to changes in air flow was investigated by stopping the air flow completely and recording temperatures daily for



Figure 5.29 Variation in heat flow for 5 days after stopping ventilation air flow.

five days. The resulting heat flows from each section are shown in F. ture 5 29. The uninsulated section showed a marked decrease in heat frow, from 91,2 to 50,5 W/m, during the five days of measurement. The insulated sections showed no definite response to stopping the air flow.

5,10.4 The effec\* footwall gravel

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The bulk ther ty of packed quartz gravel has been measured as one sixth tr. . . . . . ' rock (Wiles and Maxwell, 1959). A layer of rock 300 mm thick with ... nermal conductivity of  $0,9$  W/mK is equivalent to a 10 me layer of good insulation. However, it is not possible to detect any reduction in hear flow due to the footwall ballast by examining the heat flux from the individual rock faces (Figures 5.26 and 5.28). The average heat fluxes from the footwalls are not lower than the heat fluxes from the other rock faces, and it would appear that the footwall ballast does not have a significant effect on rock heat flow i..to tunnels.

#### 5 11 Summary

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A test site at Western Deep Levels Gold Mine was divided into th.ee sections which were

- (i) uninsulated
- (ii) fully insulated
- (iii) partially insulited.

The specification for the insulation thickness was 50 mm. However, this was not achieved in practice, the thickness varying greatly with an average of 76,9 mm.

Temperatures within the rock body at each section were recorded for 24 weeks. From this data and a knowledge of the rock thermal conductivity the heat flux at each section was calculated It was found that the average heat flow from the uninsulated section was 80,6  $W/m$ , whereas foi the partially and the fully insulated sections the average results were 56,0 W/m and 34,6 W/m respectively.
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The average reduction in heat flow as pompared with the uninsulated control section, was 56,7 per cent in the totally insulated section and  $29.7$  per cent in the partially insulated section.

In order to asse, a whether the ballast on the footwall had any insulating affect, the heat flows from the sidewalls, footwalls and hangingwalls weic compared. The heat flow ftom the footwall was not found to be consistently lower than any of the other faces, as was predicted by theory.

In the next chapter a full comparison is made between results obtained at che test site and theoretical modelling

COMPARISON OF EXPERIMENTAL AND THEORETICAL RESULTS

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## 6,1 Introduction

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The accurate experimental measurement of rock heat flow in mine excavations is a difficult undertaking. Acceptably accurate results are only possible if a careful experimental procedure is followed. Furthermore. the theoretical analysis of rock heat flow into tunnels is complex and it is usually necessary to accept some approximations. It is therefore appropriate to compare and to assess the results obtained by the two procedures

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In this chapter the results of the experiment are compared with results obtained firstly by finite element analysis which models the test conditions as accurately as possible and, secondly by simplified methods of predicting heat flow into tunnels.

# 6.2 Hinite element analysis of heat flow in the experimental \*est sections

## 6 2 1 Introduction

Numerical techniques must be used to model the test site as accurately as possible. By using the finite element method it is possible to simulate all of the following: the rectangular cross-section of the tunnel, the discontinuous boundary conditions of the partially insulated section, and the temperature field which existed before the insulation was applied

### 6 . 2 2 Finite element mesh

The know...' je acquired during the testing of the 'ADINAT' package led to the drawing up of the finite element mesh shown in Figure 6.1. The mesh consisted of 100 elements which increased in sire geometrically



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Figure 6.1 100 element mesh used for modelling the uninsulated<br>test section.



Figure 6.2 200 element mesh used for modelling the fully insulated test section.

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Figure 6.3 400 element mesh used for modelling the partially<br>inaulated test section.

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with the distance from the tunnel perimeter. The dimensions of the tunnel cross-sections are given in Table 5.2 It was only possible to use the mesh shown in Figure 6.1 for the uninsulated section which was square and had uniform boundary conditions. The 200 element mesh shown in Figure 6.2 was used for the rectangular fully insulated section For the partially insulated section it was necessary to use the large, 400 element mesh, shown in Figure 6.3.

#### 6.2.3 Test conditions

Despite the use of a numerical method of modelling the conditions at the experimental test site, it was necessary to make some assumptions and approximations. The values of parameters used in the model and any approximations that were made are described below.

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The values of rock thermal conductivity measured at the site, (Table 5.1,), were used in the analysis. The value used for each section was the average of 12 measurements of rock samples taken from around the  $\frac{1}{2}$ perimeter of the tunnel cross-section.

The virgin rock temperature was assumed (Figure 5.6) as being 42,7 "C.

The ambient air temperature was assumed to be constant at 31 °C. This value was the average of the continuous air temperature measurements that were recorded it the site.

The ventilation air flow was assumed to be constant at  $6.5$  m<sup>3</sup>/s, whereas in fact it varied considerably at the site (Figure 5.7) This assumption had the effect of giving a predicted heat flow that was smrother than that which was experimentally determined. However the overall average results are not affected and can be satisfactorily compa.ed

The average air volume was used to compute the heat transfer coefficients for the tunnel surfaces, which were evaluated as follows:

The surface heat transfer coefficient for smooth wall pipes can be found from a simple expression (Dittus and boelter, 1941) given by:

 $N_{\rm u} = 0.023$   $R_{\rm e}$ <sup>3</sup>  $P_{\rm r}$ <sup>6</sup> ((e) m

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Allowance was made for the irregular surface by multiplying the right hand side nf Equation 6.1 by a roughness factor (Nunner, 1956) The hydraulic diameter was used in evaluation of the Musselt and Reynolds numbers. Substitution of the known parameters, results in surface heat transfer coefficients of  $3,2$ ,  $3,4$ , and  $3,7$  W/m<sup>2</sup>K for the uninsulated, fully insulated and partly insulated sections prior to insulation being applied. The difference in the values of heat transfer coefficient is mainly due to the difference in hydraulic diameter at each section

The thicknesses of insulation used in the model were assumed to be constant at each section. The values were the averages of the many measurements taken at the site and were 74,9 mm for the fully insulated section, and 79,6 mm for the partially insulated section. The measured value of thermal conductivity of the insulation was 0,042 W/mK.

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The procedure described in Chapter 3 was followed to allow for the effects of the thin layer of insulation on the rock surface. An equivalent surface heat transfer coefficient was computed from a combination of the actual surface heat transfer coefficient and the thermal resistance of the insulation Following this approach yielded 0,48 and 0,47 W/m\*K for the fully and partly insulated sections respectively. The uninsulated section was unchanged, with a heat transfer coefficient of 3,2 W/m'K

 $1-c$  insulation was applie! F7 weeks after the tunnel was holed, and the effects of insulation were analysed for 24 weeks ( the duration of the experiment).

## 6.2.4 Results of finite element analysis

As the insulation was applied to the rock surfaces approximately 87 weeks after excavation of the tunnel, it was necessary to compute the temperature gradient within the rock body before proceeding to analyse the effects of the insulation. The heat flow from each section prior

to applying the insulation is shown in Figure  $6.4$ . There is little difference in heat flow between each section, indicating that a comparison between the insulated sections and the uninsulated control section was satisfactory both for the experiment and the tueoretical prediction.



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Figure 6.4 Heat flow from each test cross-suction prior to insulating as predicted by finite element analysis.

The boundary conditions were then changed, where necessary, to make allowance .or the insulated surfaces and finite element computations were made for a further 24 weeks. The computed heat flow for each section is shown in Figure 6.5 and the percentage reduction in heat flow in Figure 6.6

The average heat flow was  $138,8$  W/m for the uninsulated section, 70,1 W/m for the partially insulated section, and 39,9 W/m for the

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Reduction in heat flow at the fully and partially Figure 6.6 insulated cross-section as predicted by finite analysis

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fully insulated section. These values are equivalent to a 49,5 per cent reduction in heat flow for the partially insulated section, and 71,3 per cent for the fully insulated section

The results presented in Figure  $6.5$  can be compared directly with the measured values (Figure 5.21). The predicted heat flow of 138.8 W/m for the uninsulated section is very much higher than the measured value of 80,G W/m. Some differences between the model and the actual test conditions are due to assuming steady air flow, average rock properties and smooth rock surfaces (except for the calculation of the surface heat transfer coefficient). However, it is unlikely that these assumptions are responsible for such a large difference. The most probable reason for the difterence is that the rock was assumed to be at the virgin rock temperature on the day of excavation It is likely that due to the position of the tunne. within the shaft pillar, the rock in the region had cooled below the virgin rock temperature. Fortunately this difference does not have significant bearing on the results of the experiment, as concern was mainly with the percentage reduction in heat flow and not the actual magnitude of the heat flow.

The percentage reduction in heat flow for the fully insulated section was on average 71,3 per cent over the 24 week period The actual measured value was 56,7 per cent. For the partially insulated section the predicted reduction in heat flow was 49,5 per cent, which compares with the measured value of 29," per cent. The differences between the measured and the predicted results are most probably due to the large variation in the thickness of the insulation at the test site (see Figure 5.5). The direction of heat flow tended to follow the path of least resistance (that is through the areas of thin insulation cover ing), and resulis in a higher heat flow than that predicted by assuming a constant average thickness. As an example the effect of a varied insulation thickness was shown in Chapter 3. In the test case it was found chat the heat flow through an insulated slab was increased by 20 per cent if the insulation was not of an even thickness.

## 6.2,5 The effects of delaved insulation application

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In the analysis presented in Chapter 4, the insulation was assumed to be applied, and thus effective, from the day of holing ihrough. In

practice this would not be the case. In the case of the experiment conducted at western Deep Levels gold mine the insulation was applied 87 weeks after holing through. The effects can be jeen in Figure 6.7 which shows the hear flow from the uninsulated section, from sections with the insulation applied after 87 weeks (e repeat of Figures 6.4 and 6.5), and from sections with the insula\*.on effective from the day of holing through.



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Figure 6.7 The effect on heat flow of applying insulation 87 weeks after holing the tunnel.

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There is a marked reduction in heat flows immediately after the application of the insulation at week 87. The heat flows then increase to asymtotically approach the heat flows from the sections which were insulated from the day of holing through. By assuming the application of insulation to be on the day of holing through, the reduction in heat flow is underestimated but not by a significant amount. This result is important as it indicates that much simpler m thods of predicting the reduction in heat flow can be used with confidence.

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## 6.3 Simple analysis of heat flow into the ex; imental test sections

## 6.3 1 Introduction

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It is impractical for the engineer wishing to predict heat flow into insulated tunnels to resort to finite element analysis. It is therefore important to assess the results of the experiment and of finite element analysis against those obtained from simplified calculation techniques.

### 6.3.2 Results of simplified analysis

The most suitable method of simply predicting the heat flow into a fully insulated tunnel is by means of the tables produced by Jaeger and Chamalaun (1966). This is not possible for partially insulated tunnels due to the discontinuous boundary conditions, but the quasi-steady method can be satisfactorily employed for this purpose. Both of these techniques were explained fully in Chapter 3.



#### figure 6.8 Heat flow at each test section aa predicted by simple anaylsis

Both methods have two deficiencies. Firstly, no allowance can be made for the time period prior to the application of insulation and, secondly, the methods apply only to circular tunnels. The transistion from circular to rectangular airways is made on the assumption of equal cross sectional areas. For the partially insulated section there is no foundation for this assumption other than its general acceptance (tee Chapter 3).

The results of heat flow obtained using the test site condition!  $(Section 6.2.3)$  are shown in Figure 6.8. They compare well with the results obtained using finite element analysis (Figure 6.7), which are generally higher by approximately 6 W/m

For these type of analyses it is therefore generally unnecessary to obtain finite element solutions, the simple methods being quite adequate.

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#### 6 4 Summary

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The heat flow and the percentage reduction in heat flow due to insulation at the experimental test site were overestimated by theoretical methods. This was probably due to the assumption that the rock mass was at the virgin rock temperature on the day of excavating the tunnel, as well as to the large variation in insulation thickness.

After = short time no significant error resulted from the assumption that th nsulation was applied immediately the tunnel was holed, and this permits the simple heat flow prediction techniques to be used.

It was found that finite element analysis was generally unnecessary. The simplified methods of analysis gave results which were slightly lower than those produced using finite element analysis, but are adequate for general engineering computations

### 7 INSOLATION PROPERTIES

## 7.1 Introduction

The main aim of this dissertation was, firstly, to analyse theoretically the effects  $\gamma f$  insulation on tunnel heat flow, and secondly, to provide some data as a check on the theoretical findings. An experiment was conducted at Western Deep Levels gold mine to obtain the empirical data. However, a suitable material for mine wide application still needs to be developed. The material needs to have the properties which are outlined in this Chapter.

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It is important to note that the benefits of coating the rock surfaces are not only in the insulating effect but also in the support properties of the material. In fact, some mines are considering the complete shotcreting of all rock surfaces in the haulages and cioss-cuts as they are developed (Lloyd, 1984), irrespective of any insulating benefits. A material suitable for both support and insulation purposes would have obvious ben-fits. Additionally a smooth coating on the rock surfaces would serve to reduce the resistance to airflow and this would be manifested as savings in fan power

## 7.2 Insulation Material Properties

There are several factors which influence the choice of a suitable mine tunnel insulation material. For practical minewide application the insulation material needs to be reasonably priced (see Chapter 8) and easily available. The material must also possess the following proper' es:

### Thermal Conductivity

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The lower the conductivity, the less is the amount of material needed to have the same insulating effect. As a reference value it should be noted that polyurethane has a conductivity of  $0.03$  W/mK and it has been shown that a layer of 50 mm would be suitable for insulation purposes.

More details cf choosing an optimum insulation thickness are given in chapter 8.

#### Toxicity

During application and curing a number of insulation foams emit harmful gases. In particular, attention will be given to formaldehyde gas which is -arcinogenic and concentrations of greater than 2 ppm should be avoided.

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## Fire Resistance

It is extremely important that the insulation product does not support combustion, or produce noxious gases on burning.

#### Composition

The insulation material should not be susceptible to attack from bacteria and should be unaffected by running water or high humidity.

### Structural Strength and Durability

A high structural strength would be beneficial with regard to the shoring of rock and the prevention of spalling, as well as for good durability of the insulation surface. The product should have a good adherence to the rock.

## Case and Evenness of Application

The insulation material should be simple to apply in large quantities. The hangingwall can cause difficulties as a result of the insulation falling off before setting. Product density, hermal conductivity and application thickness should be easily controlled in an underground environment. I' carticulary important to be able to maintain the thickness of the elation within reasonable limits. Optionally the material could be supplied as panels which alleviate most of these problems

In Table 7 1 a comparison of some different insulation material is shown. Although some materials are promising, an insulation which has all the attributes required for insulating mine airways is not yet available. Many manufacturers are presently working on developing a suitable product



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## Table 7.1 Comparison of some insulation materials

NOTES: 1. Some organic binders are combustible.

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- 2 Can absorb large quantities of water unless treated with a finishing cement.
- 3. May emit toxir gases on application and for some time afterwards
- 4. Can cause problems due 10 excess fibres in the ventilation air stream

#### 8 FINANCIAL ANALYSIS

## 8.1 Introduction

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I' has been shown that significant reductions in heat flow, of the order of 50 per cent, can be achieved by full insulation of mine airways. If the footwall remains uninsulated tie reduction in heat load is less, being of the order of 25 per cent. However, for the engineer designing ventilation and refrigeration systems for deep level mines, the cost of insulating mine airways must be economically justified. The number of variables involved in evaluating tunnel heat flow are too numerous to permit a general analysis in this dissertation. However, presented below, by wa, si example, is an analysis of the cost benefits of insulation, for a particular set of underground conditions. Optimum insulation thicknesses are established for materials of various unit volume costs, and both full and partial insulation is considered.

# 8 .2 Sample Cost Benefit Analysis and Optimisation of Insulation for Deep Level Mining

As an example of the economic benefits of insulation, the cost of insulating the airway in the following hypothetical case was examined:

A heat exchanger cools 27 kg/s of ventilation air to 20 °C saturated. The air travels along a  $2,000$  m long,  $3x3$  m intake airway, to ve.tilate the mine workings. The airway is dry, and the virgin rock temperature is 50 \*C

Tn Figure 8 1 the heat pickup from the airway is shown when the tunnel is uninsulated, and fully, or partially insulated with varying thickness of insulation at a thermal conductivity of 0,03 W/mK. A tunnel age of one year was assumed.

Figure 8.2 shows the per cent reduction in heat flow as a result of full or partial insulation of the airway with varying thicknesses ofinsulation.

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 $600 -$ Uninsulated Partially insulated 400 Heat flow (kW) Fully insulated 200  $\circ$  $\frac{1}{\alpha}$ 80 100  $40$  $60$  $20$ Insulation thickness (mm)





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Figure 8.2 Variation of the percentage reduction in heat flow flow with insulation thickness

The capital cost of refrigeration plant was taken as R450/kW(R) and the running cost as R55/kW(R) per annum. For this example it was assumed that the associated refrigeration distribution system has a capital cost equal to the cost of the refrigeration plant.

To enable a direct comparison to be made between the cost of insulation and the running of refrigeration plants the 'annual cost' concept (Lambrechts and Howes, 1982) was employed. This is a method of expressing overall costs over the life of the system, based at ar appropriate interest rate, in terms of an average in one year. An 'annual cost' multiplying factor can be found in published tables (Lambrechts and Howes, 1982). For an assumed life of 10 years and an interest rate of 15 per cent th. factor is 5,02. The annual cost of supplying one k.lowatt of refrigeration on a mine is thus equal to 55+(450+450)/5,02 or 8234,3.

It is now possible to evaluate the cost benefits of insulating the 2 000 m length of tunnel. In Figures 8.3 and 8.4 the cost savings due to insulating the tunnel nartially and fully are shown for varying thicknesses of insulation for different insulation costs. For every line representing the cost of insulation it is possible to select an optimum thickness of insulation for maximum financial return. A locus has been drawn through these points and this is termed the 'locus of maximum saving'

For an insulation material costing RSOO/m) the optimum thickness for a fully insulated airway is 11 mm, which from Figure 8.2 results in a reduction in heat flow of only 23 per cent. The financial saving would be only R3 500 per annum and consequently it is doubtful whether the exercise would be viable. However, different (less expensive) materials present a much more positive view.

As an example, the price of urea formaldehyde insulation is  $R135/m<sup>3</sup>$ . When fully insulating a mine airway the optimum insulation thickness is 50 mm, with a reduction in heat flow of 59 per cent and a financial saving of R45 000 per annum. For partial insulation the optimum insulation thickness is 28 mm, with a reduction in heat flov of 29 per cent and a financial saving of  $R26000$  p.a. The savings are  $.000$ significant and it is clear that with a suitable insulation material

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and an efficient, perhaps automatic, method of application, the insulation jf mine airways can be a practical proposition for both fully and partially insulated rases

#### 9 CONCLUSIONS AND RECOMMENDATIONS

The main conclusion that can be drawn from this work is that substantial reductions in heat (low ran be realised by insulating tunnel rock surfaces

Savings are typically between 50 and 70 per cent for fully insulated dry tunnels. Significantly, if the footwall remains uninsulated these savings are reduced to between 20 and 40 per cent. Furthermore, if the fhotwall is both uninsulated and damp the reductions in heat flow are marginal; less than 20 per cent.

These values are greatly affected by the rock thermal conductivity, the tunnel dimensions (radius), ventilation air f'ow, tunnel age, tunnel length, insulation thermal conductivity and insulation thickness. Nevertheless it has been shown that simple evaluation techniques based on solutions of heat flow into circular cross-sectional tunnels can produce adequate results. Finite element analysis was used to evaluate these methods and to investigate the effects of time delays between the excavation of the tunnel ani application of the insulation, but this is not necessary for general engineering calculations.

The reduction in heat flow that can be achieved by insulating airways under a variety of condition sere computed. The results are presented as a set of nomograms in Apper D. These nomograms cover the wide range of conditions which are in South African gold mines and serve as a useful tool for the ; racticing engineer.

The experiment conducted at Wests. Deep Levels gold mine produced reductions in teat flow of 56,7 per east in the fully insulated section und 29,7 per cent in the partially insulated section. These values are less than those predicted by theory and the differences are most probably due to the large variation in the thickness of the insulation at the test site. No evidence was found of an insulating sifec. due to the footwall ballast. Theoretically the footwall ballast should go some way to alleviating the problem of an uninsulated footwall.

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It was shown that there is a clear diminishing return on increasing the thickness of the applied insulation. There is an economic optimum insulation thickness for which no *global value* can be given. However, it has been shown, by means of a typical example, that significant financial savings can be made by applying insulation priced between R100 and R200/m<sup>3</sup>. Materials are available which meet this price criterion, and techniques need to be devised for effective covering of the rock surfaces economically

If the practicing engineer is to derive benefit from this work, it is necessary to provide general recommendations as a guide to the selection and implementation of tunnel insulation There are a number of steps that must be followed and several practical problems which must be overcome. It is recommended that the following points be considered when contemplating the insulation of tunnel surfaces.

The heat flow from the prrposed network of ventilation tunnels must be evaluated. This is easily done by using one of the computer program lised in Appendix B. The heat loads from all of the airways on a mine can be computed by using a heat flow network program (Chorosz, 1986).

An estimate of the possible reductions in heat flow can be found from the nomograms in the Appendix D. If the set of nomograms do not cover the desired conditions, the reduction in heat flow can be computed from the programs in Appendix B. It can be expected that the overall reduction in heat flow will be of the order of 10 per cent for a full insulation covering. This will be nalved for partial insulation and halved again for a wet footwall.

These calculations must be followed  $\rightarrow$  an economic study based on the  $\overline{\phantom{a}}$ cost of insulation and the cost of  $\sim$  lying refrigeration. A guide to  $\sim$ the type of procedure to be follow  $\qquad \circ$  wen in Chapter 8. The results of an economic study will may be accrued, and the optimum theory is of insulation that is to be applied r the savings in Rands that

The selection of a suitable insulation, material for mine wide application requires careful consideration. A guide to desirable properties is gives in Chayter 7. In particular fire resistance, toxicity and

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thermal conductivity are important parameters. A material suitable for insulating the footwall should be sought since approximately GO per cent of the total heat flow passes through the footwall in a partially insulated tunnel. Finally a material  $\ast$  ich can be evenly applied must be used

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## APPENDIX A

## A1 The Quasi-steady Method

The published version of the quasi-steady method needs some modification before it is possible to allow for the effects of an insulated surface. In order to account for insulation on the tunnel surface the thermal capacity is ignored and an 'equivalent' surface heat transfer coefficient is calculated. This 'equivalent' surface heat transfer coefficient,  $h_{\alpha}$ , includes the effect of insulation and the convective heat transfer coefficient, h :

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insulation thickness  $\frac{1}{h}$ .  $\mathbf{h}_{\mathrm{e}}$ 

The geometry of the partially insulated airway is shown in Figure A 1. The cross-section is assumed to be circular. The uninsulated portion subtends an angle 2# at the centre of the circle.



Figure A1 Geometry of airway cross-section.

The heat transfer at the surfaces is by a combination of convection and radiation. At the bare surface tie heat flux ie given by:

$$
\frac{k\partial T}{\partial r} = h(T_S - T_{DB}) + K(T_S - T_{INS}) + f\lambda E[P_{SAT}(T_S) - P]
$$
\n
$$
(A1)
$$

while at the insulated surface:

$$
\frac{k\partial T}{\partial z} = h_e(T_s - T_{DB}) + K'(T_S - T_{UNINS})
$$
 (A2)

where

$$
K' = K(\pi - \beta) / \beta
$$

If we introduce a function  $g(\theta)_+$  which has a value one on the insulated portion and zero on the bare surface, i.e

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g(\theta) = 1 for |\theta| \ll \theta= 0 for |\theta| \to \beta
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it is possible to combine equations (A1) and A2).

Thus:

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$$
\frac{k\partial T}{\partial r} \approx g(\theta) \left[ h(T_S - T_{DB}) + K(T_S - T_{INS}) + f\lambda E(P_{SAT}(T_S) - P) \right]
$$
  
+ 
$$
\left[ 1 - g(\theta) \right] \left[ h_e(T_S - T_{DB}) + K'(T_S - T_{UNINS}) \right]
$$
(A3)

which holds on  $r = a$  for all  $\theta$ 

Now

$$
P_{SAT}(T_S) = P_{SAT}(T_{UNINS}) + (T_S - T_{UNINS}) P_{SAT}(T_{UNINS})
$$

where P' $_{\tt SAT}$  is the slope of the curve for saturated vapour pressure.

By re-arranging we obtain:

$$
\frac{(\partial T)}{(\partial r)}_{r=a} = q_1 + q_2 T_S + q_3 g(\theta) + q_4 T_S g(\theta)
$$
 (A4)

where

 $\mathbf{q}_1 = - (\mathbf{h}_\mathrm{e} \mathbf{T}_\mathrm{DB} + \mathbf{K}^\top \mathbf{T}_\mathrm{UNINS}) / \mathbf{k},$ 

$$
q_2 = (n_e + K^2)/K,
$$
  
\n
$$
q_3 = ((-hT_{DB} - KT_{INS} + h_eT_{DB} + K'T_{UNINS}) + f\lambda E (P_{SAT}(T_{UNINS}))
$$
  
\n
$$
T_{UNIHS} P_{SAT}(T_{UNINS}) - P))/k,
$$

and

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$$
q_4 = ((h + K - h_e - K') + f\lambda E P'_{SAT}(T_{UNINS})/k)
$$

Instead of solving the heat diffusion equation, we are to solve Laplace's equation given by:

 $\frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} + \frac{1}{r^2} \frac{\partial^2 T}{\partial \theta^2} = 0$ 

The general solution can be derived by the method of separation of variables and is given by:

$$
\mathbf{T}(r,\theta) = \mathbf{A}_{0} + \mathbf{A}_{0}^{\dagger} - \mathbf{1}nr + \sum_{n=1}^{\infty} (\mathbf{A}_{n}r^{n} + \mathbf{A}_{n}^{\dagger}r^{-n})\sin n\theta
$$

$$
\leftarrow \mathop{\cup}\limits_{n=1}^{\infty} (B_n r^n + B_n^+ r^{-n}) \cos n\theta
$$

If the condition imposed by the quasi-steady approach that at  $r = R$ ,  $T = T_R$  for all  $\theta$  is applied, then it can be easily shown that:

$$
T(r,\theta) = T_R + C_0 \ln(r/R) + \sum_{n=1}^{\infty} C_n \left[ (r/R)^n + (R/r)^n \right] \cos n\theta
$$
 (A5)

It only rerains to satisiy the condition given by equation (A4).

By differentiating equation (AS) at  $r = a$  we obtain

$$
\frac{(\partial T)}{(\partial T)}_{T=a} = C_0/a + \sum_{n=1}^{\infty} C_n [(n/R) (a/R)^{n-1} + (nR/a^2) (R/a)^{n-2}] \cos n\theta
$$
 (A6)

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We are only concerned with temperatures on the surface  $r = a$ .

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If we write:

$$
T_S = T(a, \theta) = T_R + A_0 + \sum_{n=1}^{\infty} A_n \cos n\theta
$$
 (A7)

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and

$$
\frac{(\frac{\partial T}{\partial r})}{(\frac{\partial T}{\partial r})_{r=a}} = \lambda_0 \gamma_0 + \sum_{n=1}^{m} A_n \gamma_n \cos n\theta
$$
 (A8)

then by comparison with equation (A5) and (A6) it can be shown that:

$$
\gamma_n = 1/\{a \ln(a/\hbar)\}
$$

and

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$$
\gamma_n = (n/a) \left( (a/R)^{2n} + 1 \right) / \left( (a/R)^{2n} - 1 \right)
$$
 (A9)

for

 $n = 1, 2, ...$ 

It is then sufficient to find values of  $\mathtt{A_0},\mathtt{A_1},$  ...... without evaluating  $C_0$ ,  $C_1$ , .....

By expanding the function  $g(\theta)$  in a Fourier series from -  $\pi$  to  $\pi$  we can write:

$$
g(\theta) = B_0 + \sum_{n=1}^{n} B_n \text{ Cosne}
$$
 (A10)

where  $B_0 = \beta/\pi$ 

and 
$$
B_n = (2/n\pi) \sin n\theta
$$

substituting  $A(7)$ ,  $A(8)$ , and  $A(10)$  into  $A(4)$  gives  $\mathbf{A}^{\mathcal{N}}_{\mathcal{O}} + \sum_{\mathbf{A}^{\mathcal{N}}_{\mathbf{A}}} \mathbf{C} \circ \mathbf{S} \mathbf{n}^{\mathcal{O}} = q_{\mathcal{N}} + q_{\mathcal{Z}} \left( \mathbf{T}_{\mathbf{R}} + \mathbf{A}^{\mathcal{O}}_{\mathcal{O}} + \sum_{\mathbf{A}^{\mathcal{O}}_{\mathbf{A}}} \mathbf{C} \circ \mathbf{S} \right)$ + q<sub>3</sub> ( $B_0$  +  $\sum B_n$  Cos ne) + q<sub>k</sub>  $(P_0 + E B_p \cos n\theta) (T_R + A_0$ +  $\sum A_n \cos n\theta$ 

Which, by comparing like terms in Cos n8 for n=0,1,2.... N leads to  $\alpha$ set of linear equations. These equations can be expressed as:

$$
\sum_{n=0}^{N} G_{mn} A_n = C_m \qquad m = 0, 1, 2, \dots, N \tag{A11}
$$

where

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$$
C_0 = q_1 + q_2 T_R + B_0 (q_3 + q_4 T_R)
$$
  
\n
$$
G_{00} = \gamma_0 - q_2 - q_4 B_0
$$
  
\nif n  $\diamond$  0  
\n
$$
C_m = B_m (q_3 + q_4 T_R)
$$
  
\n
$$
G_{m0} = -q_4 B_R
$$
  
\n
$$
G_{m0} = \gamma_m - q_2 - q_4 B_0 - q_4 B_{2n}/2
$$
  
\nif m  $\diamond$  0  
\n
$$
G_{0n} = q_4 B_n/2
$$
  
\nand if both  $\gamma$   $\diamond$  0 and m  $\diamond$  0

$$
G_{mn} = -q_*(B_{n+m} + B_{n-m})/2
$$

By solving this system of equations the A coefficients can be found and hence the rock surface temperature from equation (A7). An iterative algorithm, presenting a method of solution is shown in Figure Improved values of average temperature for the uninsulated and insulated surfaces axa given by:

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$$
T_{UNINS} = T_R + A_0 - \sum_{n=1}^{N} [A_n/n(\pi - \beta)] \sin n\beta
$$
 (A12)

and

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$$
T_{INS} = T_R + A_0 + \sum_{n=1}^{N} (A_n/n\beta) \sin n\beta
$$
 (A13)

respectively

The heat transfer can then be found by summing the results from equations (A1) and (A2).

## A2 An Integration Algorithm

To find the total heat transfer from the rock to the ventilation air c/er a finite length of tunnel a stepping method is used. The total length of airway is divided into short sections O'er which conditions are assumed to be constant. Changes in air temperature can then be incrementally evaluated, the condition of outlet air from one section being used as the inlet condition for the subsequent section.

A complete listing of a computer program which implem ,ts both the quasi-steady method and the above stepping procedure is given in Appendix 8

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## Computer Programs

The full listings of two computer programs used for the calculation of heat flow into insulated tunnels are presented in this appendix.

The first program was used for calculating heat flow into uninsulated or fully insulated tannels, and is based on the published tables of Jaeger and Chamaiaun. The second program was used for calculating heat flow into partially insulated airways and is based on the quasi-steadymethod.

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 $10$  $\rightarrow$   $\rightarrow$   $\rightarrow$   $\rightarrow$   $\rightarrow$   $\rightarrow$   $\rightarrow$ **I ROUTINE TO CALCULATE HEAT FLOW FROM UINSULATED & FULLY INSULATED**  $\hat{z}$ 0  $38$  $\mathbf{r}$ AIRWAYS. SEE:JAEGER, J.C. & CHAMALAUN, T. HEAT FLOW IN AN INFINITE REGION  $\overline{AB}$ BOUNDED EXTERNALLY BY A CIRCULAR CYLINDER WITH FORCED CONVECTION AT THE SURFACE. MET. NOV-DEC 1983. 50  $60$  $\rightarrow$ 8UST.J.PHYS.,1966 70 ! AUTHOR: P. BOTTOMLEY  $88$ CHAMBER OF MINES RESERRCH LABORATORIES 98 P.O.BOX 91230  $100$  $\mathbf{r}$ AUKLAND PARK 2006  $110$ **. \***  $120$ PRINTER IS 16 130  $140$  $150$ 1.1/0 Routine .......Input Parameters.  $160$ 一一分的的的名词形式和名词形式和名词形式由的现在分词在对方的名词形式的复数形式或名词形式或名词形式或词形式使使使物物的现在分词  $170$ PRINT PAGE PRINT "ROCK CONDUCTIVITY (W/M DEG.C)?"  $180$  $190$ INPUT Cond  $200$ PRINT "ROCK DIFFUSIVITY (M\*\*2/S)?" INPUT Diffus 210 PRINT "INSULATION CONDUCTIVITY (W.M.DEG.C)?" 220  $230$ INPUT K) PRINT "INSULATION THICKNESS (mm)?"  $240$ **INPUT Thick** 250 260 PRINT "DRY-BULE TEMPERATURE <DEG.C>?" 270 INPUT Air PRINT "BARONETRIC PRESSURE (KPa) ?"  $288$ 290 **IHPUT Pressure** PRINT "AIR QUANTITY (M\*\*3/5)?" 360 INPUT Volume 310  $320$ PRINT "VIRGIN ROCK TEMPERATURE (DEG.C) ?" **INPUT Vrt** 330 PRINT "AIRWAY AGE (YEARS : "" 340  $350$ INPUT Yrs 360 PRINT "AIRWAY RADIUS <M>?" **INPUT R&**  $370$ PRINT "LENGTH OF AIRNAY (M) ?" 380 390 INPUT Km PRINT "NUMBER OF STEPS?" 400 **INPUT Steps**  $410$ 

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 $770$ 780 1. Main Routine.  $790$ 808 Maxiter=100  $Bb = FMGoch(D) + fhus + 24 + 365 + 3600 + Yrs \wedge (Aa + Aa) + ...$ 810 *Ilbermal* Gradient 820  $Bb = Aa + E \times P (1 - Bb)$ 838  $N = 15$ THo Of Summation Step: Alfa-(1-Alfa)+PI  $040$ 850 **GOSUB** Boald *IB Coefficients*  $8\,6\,0$ Hr ad=Hr ad<Cond 870 Hrad2=Hrad\*(PI-Alfa)/Alfa thir velocity Velocity=Volume/(PI\*Aa\*Aa) 880 ilnsulation Equivalent h.t.c 890 Hc. \*Ki\*1000/Thick 900 **IStep Tength** Dx=Km/Steps 910  $Sens t = 0$  $920$ 930 I Compute Airflow In Kg/s.  $940$  $950$ Rshi=622+FNP(Wet,Air,Pressure)/(Pressure-FNP(Wet,Air,Pressure)) Density=(Pressure-FNP(Wet,Air,Pressure))/(.267045\*(273.15+Air)) 960 970 Mass=Density\*PI\*Aa\*Aa\*Velocity (Compute Gamma Coefficients. 980 GOSUB Gamcaic 998  $1989$ 1. Step Along Airway,  $1010$ المستوين FOR Istep=1 TO Steps 1029 1838 1040 1. Compute Surface hitici- $1050$ Density=(Pressure-FNP(Wet, Air, Pressure))/(,282045\*(273,15+Air))  $1868$ 1070  $Kax(24, 2+, 075*Atr) + 1E-3$ 1090 Ku=(16.2+.084\*Air)\*1E-3 1090 Ep=PNP(Wet, Air, Pressure)/Pressure  $Rircond=(3,07*(1-Ep)*Ka+2,62*Ep*Ku)/(3.07-.45*Ep)$  $1188$ Crain=1005+1884\*.662+FNP(Wet, Air, Pressure)/(Pressure-FNP(Wet, Air, Pressure 1110  $\rightarrow$ 1120  $DiffF$ usion=1.192E-7\*(Air+273.15)^1.75/Pressure  $Viscostity = 4.74E - 8*H + r*1.716E - 5$  $1138$ Re=2\*Velocity\*Aa\*(Density/1.2)/Viscosity 1140 1150 Hcl\*.02\*Ren.8\*Aircond/(Aa\*2) Euan=Hc1/Cpair\*(Cpair\*Densitu\*Diffusion/Aircond)^(2/3)\*622/P 1160 sure  $1178$ 1 . . . . . *. . .* . 1180 I Compute Equivalent hitic. 1190 1200  $He2=1/(1/He1+1/He1)$ Hc1=Hc1/Cond 1210 1220 Hc2=Hc2/Cond 1230 02=Hc2+Hrad I Ist. Guess Ruenage Sunface Temp. 1240 Vbotn=Air 1250 Vtopn=Air 1260 Lat=2501-2.387\*Wet 1270 Cc=Lat+Evap/Cond  $C = Weet f + Cc$ 1280

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1290 1300 I Iteration Loop For Surface Templ  $\hat{\mathbf{F}}$  , where  $\hat{\mathbf{F}}$  are  $\hat{\mathbf{F}}$  $1218$ 1320 Indel 1330 Iter: Vtop=Vtopn  $1340$ **VhotsVhotn** 1350 Ps at d=FNPs at (Vbat ) +17, 27+237, 3 // 237, 3+Vbot + 2 1360 Q1 =- Hc2\*Air-Hrad\*Vbot 1370 04=Hc1-Hc2-Hr ad+Hr ad2+C+Psatd  $1388$ Q3=~Hc1\*Atr-Hrad2-Vtop+Hc2\*Atr+Hrad+'bot+C++FHPsat+Vbot+-Vbot+Psatd-FNP(W et, Air, Pressure)). 1390 GOSUE Coeffcalc !Compute C AND G Coeffic ents. 1400 1Solile Equations. GOSUB Linsolve ICompute Average Temp.  $1410$  $GOSL \times B \cup \epsilon + \epsilon m p$ . 1420 IF (ABS(Vtopn-Vtop)(1) AND (ABS(Vbotn-Vbot)(1) THEN Ind=0 1430 IF Ind=0 THEN Heatsum 1440  $Ind*Ind*1$  $1450$ IF Ind=Maxiter THEN Fail 1460 GOTO Iter  $\frac{1}{2}$  . A monoton monoton and  $\frac{1}{2}$  $1470$ 1488 + No Convergence 1498 **I** assumed 1500 Fail: PRINTER 15 0 PRINT "Maximum number of iterations e ceeded - no convengence" 1518 PRINTER IS 16 1520 GOTO End 1530 1540 1550 Heatsuml! Calculate Heat Transfer For This Section And Sum. 1568 1570 PRINTER IS 0 Sens=2\*Cond\*Aa+(Hc1\*Alfa\*(Vbotn=Air)+Hc2\*(PI=Alfa)+(Vtopn=Air))/1000\*Dx 1589 1598 Dmoist=Dx+Alfa+2+Aa+E=ap+Wetf\*(FNPsat-Vbot)-FNP(Wet, Air, Pressure))  $1607$ Rsho=Rshi+Dmo:st Mass 1610 Hir=Bir+Sens://Mass+Cpair-1000) Lath=Dmoist\*(2501-2.387\*Wet)/1000  $1628$  $1630$ Senst=Senst+Sens+Lath 1640  $D$ ist=Istep\*D× PRINT USING 1660; Dist. Air, Wet, Sens, Senst 1650  $1660$ IMAGE 5X, 4D. D, 2(7%, DD. D), 7X, 5D. DD. 6%, 6D. DD  $\mathbf{1}$  . In which 1670 . . . . . . . . . .  $1680$ # Compute Inlet M.D.To Hext Section Using HENTON-RAPHSON lieration 1698 1700 Tubg=Wet+.5 1710 Ft=FNPsat(Tubg)-.000644+Pressure+(Air-Tubg)-Pressure+Asho/(622+Asho)<br>Ftd=FNPsat(Tubg)+-17.27/(237.3+Tubg)-17.27+Tubg/(237.3+Tubg)/T1+.000644\*P  $1728$ ressure 1730 Wet=Tubg-Ft/Ftd 1748 IF ABS(Ft/Ftd)(101 THEN 1770 1750 Tubg=Wet 1760 GOTO 1710 1770 **Rshi=Asho** 1780 **NEXT Isten** PRINT LIN(2)  $1790$ 1800 End: STOP 1810 1820 Avetempt! Calculates The Average Temperatures Of The Two Surfaces. 1830  $\pm$  . We now a new parameter of the second se 1848  $7$ erm=0 FOR I=1 TO H 1850 1860 Term=Term+A(I)\*SIN(I+Alfa)/I 1870 NEXT I 1880 Vbotn=Vrt+A(0)+Term/Alfa 1890 Vtopn=Vbotn 1900 IF AlfaCPI THEN Vropn=Vrt+AC0)-Term:CPI-Alfa) 1910 RE TURN

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1920  $+$  \*\*\*\*\*\*\*\*\*\*\*\*\*\*\*\*\*\*\* 1930 Coeffcalct! Sets Up The Coefficients For The Set Of Linear Equations That L ead To The Fourier Series Coefficients Of The Final Solution For Temperature 1940 1950  $G(0,N+1)=01+02*Vrt+B(0)*(03+04*Vrt)$  $G(\theta, \theta) = Gam(\theta) - Q2 - Q4*B(\theta)$ 1960  $.970$ FOR 1=1 TO N 1980  $G(1,N+1)=B(1)+(03+04+Vrt)$ 1998  $G(1, 0) = -04*B(1)$  $2000$  $G(0,1)=-.5*04*B(1)$ 2010 FOR J=1 TO N 2020  $Term = -5*04*B (ABS(1-J))$ IF I=J THEN Term=Gam(J)-02-04\*B<B) 2930  $2040$  $G(I, J) = Term-, 5*B(I+J)*04$ 2050 NEXT J 2060 NEXT I 2070 RETURN 2090 2090 Gamcalc: | Calculates Gamma Terms. 2100  $\mathbf{I}$ ................................  $2110$ Ratio=Bb/Aa\*(Bb/Aa) 2126 Term=Ratio 2130 Gam(0)=1/(Aa\*LOG(Aa/Bb)) 2140 FOR 1=1 TO N 2150 Gam(I)=I/Aa\*(1+Term)/(1-Term) 2160 Term=Term\*Ratio 2170 NEXT I **RETURN** 2180 2190 Bealett Calculates The B Coefficients For The Funtion G(Theta). 2200 2210 \*\*\*\*\*\*  $B(0)=A1fa/PI$ 2220 2230 FOR 1=1 TO 2\*H 2240 B(I)=2\*SIN(I\*Alfa)/(I\*PI) 2250 NEXT 1 **RETURN** 2260

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rģ. 水気が.  $\mathcal{L}_0^{\mu}+\frac{\partial^2}{\partial r^2}\mathcal{L}_1^{\mu}$  by 2270 2280 Linsolve:! Solves The Set Of Linear Equations For The Fourier Coefficients Of The Solution Temperature Using Gaussian Elimination. 2298 2300 Holus=N+1  $2310$ FOR K=0 TO N-1 2320 Store=K Max=ABS(G(K,K)) 2330 2340 FOR 1=K+1 TO N 2350 IF ABS(G(I,K))(=Max THEN 2380 2360  $MaxABSCG(I,K))$ 2378  $Storefl$ 2380 NEXT I 2390 IF Store=K THEN 2450 FOR I=K TO Nplus 2480 2410  $Max*G(K, I)$ 2420  $G(K, I) = G(Store, I)$  $2430$ G(Store, I)=Max 2440 NEXT I 2450 FOR 1=K+1 TO N 2460 FOR J=K>1 TO Nplus  $G(1, J) = G(1, J) - G(1, K) + G(K, J)$  /  $G(K, K)$ 2473 2488 NEXT J 2498 NEXT I 2500 NEXT K 2510 A(N)=G(N, Nplus)/G(N, N) 2520 FOR 1=1 TO N 2530  $N + M - I$  $Sum = G(Ni, Np1us)$ 2540  $FOP$   $J=1$   $T0$   $I$ 2550 2560  $Nj$  # $N-J+1$ 2570 Sum=Sum-G(Hi, Nj)+A(Nj) 2580 **ACNIDESUM/GCNI, NID** 2590 NEXT J 2600 NEXT I 2610 RETURN

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2620 I Compute Goch Patterson Thermal Gradient Using A Polynomial Approx. 2630 2640  $\mathbf{A}$ DEF FNGoch(Alpha) 2650 2668  $Z = LGT$  $(Alpha)$ Goch=1.017+.7288\*Z+.1459\*Z\*Z-.01572\*Z-3-.004525\*Z-4+.001073\*Z-5 2670 2680 Goch=1/Goch 2690 IF Alpha<1.5 THEN Time 2700 RETURN Goch 2710 2720 I Time Period Too Short, 2730 2740 Time: PRINTER IS 0 2750 PRINT "TIME TOO SMALL - THESE RESULTS ARE TOTALLY UNRELIABLE" 2760 PRINTER IS 16  $2778$ RETURN Goch 2780 FNEND 2790 END 2800 ! SATURATED VAPOUR PRESSURE 2810 2820 3. "要想要继续跟你学生的事实有着有事是有事的的生活的学生的事实的是不会不正在的也不会不是什么事实的是不是什么是不会不会不 2830 DEF FHPsat(X)  $Psat=.6105*EXP(17,27*X/(237,3*X))$ 2840 RETURN Psat  $-850$ 2860 **FNEND** 2878 ! Vapour Pressure 2020 2890 DEF FNP(W, D, P) 2900 2910 Puair=(FHPsat(W)+(371.4+.24+D-.6\*W)-.24\*(D-W)\*P) < 371.4+.04\*D-.4\*W) RETURN Puatr 2920 2930 FHEND 2940 END

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# APPEHDIX C

# Cl Detailed Analysis of Radiation Heat Exchange in a Tunnel Cross section

In a ventilation airway heat transfer due to radiation takes place between the rock surfaces and the ventilation air, and also between rock surfaces which are at different temperatures, for example in airways with partially wet surfaces or with partially insulated surfaces. The overall radiation heat exchange process is shown in Figure 4.7 In oider to analyse the radiation heat exchange the 'radiation equivalent network method' is used (Oppenheim, 1956). The basis of the method is that an analogy is drawn between the radiation heat transfer process and an electrical equivalent. The heat flow is considered as the current, the difference in radiosity as the potential difference and othei terms are expressed as an electrical resistance. A full explanation can be found in many texts (Kolman, 1981).

Referring to Figure 4.7, the energy leaving surface 1 which is transmitted through the air and arrives at surface 2 is given by

 $J_1A_1F_12\tau$ , (C1)

and similarly that which leaves surface 2 and arrives at surface 1 is;

 $J_2A_2F_2 + T$  (C2)

 $J_i$  js the radiosity or the total radiation leaving surface i per unit time per unit area,

 $A_i$  is the area of surface i,

- $F_{ij}$  is the geometric view factor or the fraction of energy leaving surface i chat reaches surface j,
- $^{\mathsf{T}}$ a 1% the fraction of radiation leaving the surface which is txansmitted by the air stream.

Therefore the net heat exchange between the two radiating surfaces isgiven by



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By Kirchoff's identity for a non-reflecting medium the emissivity is equal to the absorptivity.

$$
\varepsilon_n = \alpha_n \tag{C4}
$$

so that

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 $\epsilon_{\rm a}$  +  $\tau_{\rm a}$  = 1 (C5)

where  $\epsilon_{\bar{a}}$  is the emissivity of the air, and  $\alpha_A$  is the absorptivity of the air.

The radiative reciprocity relation states that

$$
A_1F_{12} = A_2F_{21}
$$
 (C6)

 $\sim 3.5\, \times$ 

 $\frac{d}{d\mu} = \frac{1}{\lambda} \frac{d\mu}{d\mu}$ 4,354

and therefore by substiteting Equations C5 and C6 in Equation C3 we obtain

$$
q_{12} = A_1 F_{12} (1 - \epsilon_{\alpha}) (J_1 - J_2) \tag{C7}
$$

Using the electrical analogy Equation C7 can be represented by the network element shown in Figure C1.

Considering the energy exchange between surface 1 and the ventilation air, the energy emission from the ventilation air (other than that which is transmitted, and has already been considered) is given by the Stefan-Boltzmann law aa

$$
J_a = \epsilon_a \sigma T_a^b \tag{C8}
$$

where  $\sigma$  is the Stefan-Boltzmann constant (5,699x10<sup>-8</sup> W/m<sup>2</sup> K<sup>4</sup>), and  $T_A$  is the absolute bulk air temperature.

The fraction of this energy which reaches surface 1 is given by

$$
A_{\mathbf{a}} \mathbf{F}_{\mathbf{a}} \cdot \mathbf{r}_{\mathbf{a}} \sigma \mathbf{T}_{\mathbf{a}}^{\mathbf{t}} \tag{C9}
$$

At the same time the energy absorbed by the ventilation air from surface 1 is given by

$$
J_1A_1F_{1_A}a_A
$$
 (C10)

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$$
J_1A_1F_1{}_{\underline{a}}\epsilon_{\underline{a}}\tag{C11}
$$

The net energy interchange between the air and surface  $t$  is given by

$$
q_{\underline{a}^1} = A_{\underline{a}} F_{\underline{a}} \epsilon_{\underline{a}} \sigma T_{\underline{a}}^4 = J_1 A_1 F_{1_{\underline{a}}} \epsilon_{\underline{a}}
$$
\n
$$
(C12)
$$

Again using the reciprocity relation to simplify Equation C12 we obtain

$$
q_{\underline{A}}t = A_f F_{\underline{A}} \underline{e}_{\underline{A}} (\sigma T_{\underline{A}}^{\underline{A}} \sigma T_{\underline{A}})
$$
 (C13)

The similar relationship for the interchange between surface 2 and the air is given by

$$
q_{\underline{a}}^2 = A_2 F_{\underline{a}} \epsilon_{\underline{a}}^{\dagger} (\sigma T_{\underline{a}}^{\underline{b}} - J_2)
$$
 (C14)

This radiation exchange can also be represented by an electrical equivalent and is shown in Figure C2.

For a reflecting solid which does not transmit energy

 $\varrho + \varepsilon = 1$  ( C15 )

where  $\rho$  is the reflectivity,

and further the radiosity is the sum of the energy emitted and the energy reflected, that is



Figure Cl

Network element for the radiation transmitted<br>through the air.

 $9.96\%$   $2.94\%$ 

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Figure C2 Network element for the radiation exchange between<br>air and the surface.



Figure C3

Neiwork element for the surface resistance.



Figure C4

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Total network for the radiation heat exchange process in a tunnel containing an assorbing gas.

### $J = \epsilon \sigma T^4 + \rho G$

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 $(C16)$ 

where G is the irradiation, or the total radiation incident upon a surface, per unit time, per unit area.

By substituting Equation 15 into Equation 16 we obtain

$$
J = \epsilon \sigma T^4 + (1 \epsilon)G \tag{C17}
$$

Now the net radiation leaving a surface is the difference between the radiosity and the irradiation:

$$
q = A(J - G) \tag{C18}
$$

by eliminating the irradiation, by subsitution of Equation C17 in equation C18, the net radiation heat transfer is given by

$$
\frac{e}{q} = \frac{\epsilon \lambda}{1 - \epsilon} \left( \sigma T^4 - J \right),\tag{C19}
$$

which is represented by the network shown in Figure C3.

It is possible to combine the networks represented in Figures Cl, C2 and C3, to produce the network for the whole energy exchange as shown in Figure C4. The components of radiation heat flow in ventilation tunnels can be simply found by obtaining the solution for this network.

The net heat transfer between surfaces 1 and 2 is given by

 $q = \sigma(T^*_{1} - T^*_{2})/ER$  (C20)

where the equivalent network resistance,  $R_{\uparrow}$ , is

$$
R_T = (1-\epsilon)/\epsilon A_1 + 1/(A_1 F_{12}(1-\epsilon_{\underline{a}}) + A_1 A_2 F_{1\underline{a}} F_{2\underline{a}} \epsilon_{\underline{a}}/(A_1 F_{1\underline{a}} + A_2 F_{2\underline{a}})) + (1-\epsilon)/\epsilon A_2
$$
\n(221)

An example will now be solved to investigate the magnitude of radiation heat transfer in mine airways.

#### EXAMPLE

It was assumed that a 3x3 m airway was ventilated with air at a temperature of 30 \*C dry bulb, 25 \*C wet-bulb and a barometric pressure of 100 kPa. The mean footwall rock surface was 35 °C and the remaining rock surfaces were 32 "C.

The evaluation of view factors can be smplicated and lead to errors. In fact it is not necessary to evaluate the view factors for this type of problem, rather the 'crossed-string' method of determining exchange areas (AF) is used (Hottel and Sarofim, 1967). It should be noted that by the reciprocity relation the exchange area holds for each energy exchange. The 'crossed-string' method is suitable when surfaces have (Gray and Müller, 1960):

(a) lengths much greater than their widths, (b) constant cross-sections normal to their lengths, and (c) constant separation along their lengths.

These rules are all true of the idealized ventilation tunnel. In Figure CS. representing the tunnel cross-section, the exchange area between the two surfaces A und B given by the 'crossed-string' method is

### $AF = (L_1 + L_2 - L_3 - L_4)/2$

For the tunnel cross section  $L_1$  and  $L_4$  are equal to zero and hence  $L_1$ equals L; For unit length of tunnel che exchange area is therefore equivalent to the distance between the two end points of one of the surfaces. In this case

#### $AF = 3 m<sup>2</sup>$

The omissivity of the gases in ventilation air depend upon their partial pressure and mean beam length, and can be found from charts Most gases are transparent to radiation, the only ones in normal air which are of concern are carbon dioxide and water vapour. The percentage volume of carbon dioxide in normal air is typically very low, 0,03 per cent (Mayhew and Rodgers, 19S8), and thus has a very low partial pressure so that the raliation effects can be neglected for all



Figure C5

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'Crossed-strings' for evaluation of the radiation<br>exchange areas in a square tunnel

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Figure C6

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Emissivity of water vapour

practical purposes The partial pressure of water vapour at 25 "C wb, 30 \*C db and 100 kla was derived from psychroeetric cliarts as 2,8 kPa (Barenbrug).

The mean beam length is given by (Holman,  $1981$ ):

 $L_a = 3,6$  V/A

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where V is the total volume of gas and A is the total surface area. Therefore, in this case the mean beam length is 2,7 a.

The relation between mean beam length, partial pressure and emissivity fo, water vapour at 30  $^{\circ}$ C and 100 kPa is shown in Figure C6. This chart was derived from previously published data (Hottel and Sarofim, 1967), For a value of 7,6 kN/m the emissivity of water vapour is 0,18. It is interesting to note that an emissivity of 0,4 was quoted in the literature (Starfield and Dickson, 1967). This value corresponds to 56 kN/m and cannot be justified in normal mining conditions.

The emissivity of rock surfaces was assumed to be 0,95 (Whillier, 1182),

The resistances shown in Figure C4 were evaluated as follows:

 $\frac{1-\epsilon}{\epsilon A_2} = 0,018$  $\frac{1-\varepsilon}{\varepsilon h} = 0,006$ 

$$
\frac{1}{\lambda_1 F_{12}(1-\epsilon_a)} = 0,407 \qquad \frac{1}{\lambda_1 F_{1a}\epsilon_a} = \frac{1}{\lambda_2 F_{2a}\epsilon_a} = 1,852
$$

The equivalent resistance of the networks in parallel is equal to 0, 367 and thus the total resistance is 0,391.



Figure C7 Network for the radiation heat exchange process in a tunnel containing a transport medium.

The total heat transfer between surfaces 1 and 2 is found from equation 20, and in equal to 50,2 W. This quantity of heat radiation is surpriainqly high when considering that the heat flow due to convection r. a similar tunnel would be of the order of 100 W/m. If it is assumed that the ventilation air is transparent to radiation, the equivalent network is that shown in Figure C7, the total resistance ,IR, is given by

$$
ER = (1-\varepsilon)/\varepsilon A_1 + 1/A_1F_{12} + (1-\varepsilon)/\varepsilon A_2
$$
 (C22)

and the heat transfer between the two surfaces is given by

$$
q = \sigma(T_1^4 - T_2^4) / ER
$$
 (C23)

which is equivalent, in this case, to 55,1 W.

It is now clear that' although a large amount of heat is transferred between the two surfaces the effect upon the ventilation air is only 4,9 V

### C2 Simplified Analysis

in tne preceeding analysis it has been shown that the effect of radiation on the ventilation air is small, and it is doubtful whether the complex approach described is necessary for day to day engineering calculations. This is doubtful when it is considered that the analysis is hased on a highty idealized set of conditions. It is convenient for most computations to use the Stefan Boltzmann relation (Whillier, 1982)

$$
q = A_{\gamma} F_{\alpha\gamma} (T_{\gamma}^{\alpha} - T_{\gamma}^{\alpha})
$$
 (C24)

where  $F_{ey}$  is a combined emissivity and view factor.

By comparing Equations (20) and (24) it can be seen that

 $F_{av} = 1/A_1R_{T}$  (C25)

with a value for the example of 0,85.

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A linearized lorm of the Stefan Boltzmann equation is often used;

$$
q = h_p A F_{av}(t_1 - t_2)
$$
 (C26)

where  $h_R$  is the radiative heat transfer coefficient. Values of  $h_R$ can b ' computed from

$$
h_n = 4,62(1+(t_1+t_2)/545,3)^3
$$
 (C27)

The linearized form of the equation is as accurate as the Stefan-Boltzmann equation and often greatly simplifies the calculation of heat flow into "-"nnels. This form of the equation has been used by several authors when proposing methods for the solution of tunnel heat flow (Hemp, 1985; Starfield and Bleloch, 1983}.

When calculating the heat load on the ventilation air stream que to radiation some care needs to be exercised in evaluating  $F_{ey}$  when applying Equations C25 or C26. We have seen that a value of 0,85 is typical for the radiation between the two rock surfaces. However, the value for energy interchange between the rock surfaces and the air stre\m is quiet different, and is given by

 $F_{\mu\nu} = 1/A_1 ER - 1/A_1R_T$ 

For the example described the effective view factor between the rock surfaces and the vertilation air has a value of  $0,08$ . The effective view factor has been incorrectly evaluated in the past, with values of the order of unity being assumed (Hemp, 1985).

### C3 Conclusions

It has been shown that it is unnecessary to employ a more rigorous treatment of the effects of radiation heat transfer than that normally used when evaluating heat flow into mine workings. The contribution of radiation heat transfer to the overall heat luad is a small portion of the total, and errors incurred by applying a simple method of analysis are not significant.

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# APPENDIX D

## Nomograms showing reduction in heat flow due to insulation

In this Appendix the theoretically predicted reduction in heat flow due to insulation is presented in the form of nomograms The nomograms are for fully insulated, partially insulated and partially uninsulated with a damp footwall. Each nomogram includes the effects of variations in ventilation air velocity, tunnel age and tunnel length. In addition different nomograms are presented for variations in tunnel sise, rock thermal conductivity, insulation thermal resistance, footwall wetness and ventilation air humidity





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Reduction in heat flow for fully insulated tunnels -<br>insulation thermal resistance  $3,33$  m<sup>2</sup>K/W

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Reduction in heat flow for fully insulated tunnels<br>- rock thermal conductivity 3,0 W/mK. Fiqure D6





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Figure D10 Reduction in heat flow for fully insulated tunnels<br>- tunnel radius 2,82 m.

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Partially insulated tunnel Rock thermal conductivity  $= 6.14$  W/mk Tunnel radius  $= 1,69$  m Insulation thermal resistance  $\approx 1.67 \text{ m}^2 \text{k} / \text{W}$ 



Figure D11 Reduction in heat flow for partially insulated  $t$  unnels  $\sim$  average conditions.

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Partially insulated tunnel<br>Rock thermal conductivity=6,14 W/mk Tunnel radius  $= 1,69$  m Insulation thermal resistance =  $0.33 \text{ m}^2 \text{k/W}$ 











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Partially insulated tunnel Rock thermal conductivity  $= 6,14$  W/mk Tunnel radius  $\approx 1,69$  m Insulation thermal resistance  $= 3.33$  m<sup>2</sup>k/W

Air velocity (m/s)

Air velocity (m/s)

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Partially insulated tunnel Rock thermal conductivity  $\approx 6,14$  W/mk Tunnel radius =  $1,69$  m Insulation thermal resistance =  $5,00$  m<sup>2</sup>k/W

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Air velocity (m/s)

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Figure D18 Reduction in heat flow for partially insulated  $t$ unnels - tunnel radius  $1, 13$  m.

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Air velocity (m/s)

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Figure D20. Reduction in heat flow for partially insulated.<br>tunnels – cunnel radius 2,82 m.

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Partially insulated tunnel Wetness factor  $= 0.2$ Relative humidity = 50% Rock thermal conductivity  $\approx 6.14$  W/mk Tunnel radius = 1,69 m Insulation thermal resistance =  $1,67$  m<sup>2</sup>k/W



Figure D21 Reduction in heat flow for partially insulated<br>tunnels - wetness  $0.2 -$  humidity 50 %.

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Partially insulated tunnel Wetness factor =  $0.2$ Relative humidity =  $75%$ Rock thermal conductivity=6.14 W/mk Tunnel radius  $= 1,69$  m insulation thermal resistance =  $1.67 \text{ m}^2 \text{k/W}$ 



Figure D24 Reduction in heat flow for partially insulated<br>tunnels - wetness 0,2 - humidity 75 %.
Partially insulated tunnel Wetness factor =  $0,5$ Relative humidity  $= 75\%$ Rock thermal conductivity=6,14 W/mk Tunnel radius  $\approx 1.69$  m insulation thermal resistance =  $1.67 \text{ m}^2 \text{k/W}$ 





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Figure  $\geq$  6 Reduction in heat flow for partially insulated<br>tunnels - wetness 1,0 - humidity 50 %.

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